

SIMULATION MODEL OF THERMAL WATER DISCHARGE EFFLUENT FROM THE STEAM ELECTRICAL GENERATING POWER PLANT "TAMBAK LOROK" AT TANJUNG EMAS HARBOR POND SEMARANG

Sunarsih

Faculty of Science and Mathematics, Diponegoro University
Research Centre for Technology Development, Research Institute of Diponegoro University
Gd. Widya Puraya Lantai II Tembalang Semarang, Central Java - Indonesia

ABSTRACT

Simulation model is built for simulating the residual chillier which has now become hot water discarded through an outlet to Tanjung Emas harbor pond. The discarded water is called "thermal effluent" and will cause changes in sea temperature in the surrounding areas.

The figuring of the causal relationship among those factors is carried out by developing a subsystem model and building it from the model's subsystems to make a big system. It shows the complexity of the water effluent model. To know the immensity of the effects of each factor and relationship with the simulation of the model, one chooses an approach in the analytical method of dynamic system which uses the program "Powersim version 2.01" copyright 1993 - 1995 by ModelData U.S.A.

The result of model simulation showed that the temperature effect on the physical-chemical characteristics will improve the water condition with diversity index and will decrease according to the temperature condition with respect to time.

Keywords : Simulation model, thermal effluent, diversity index.

I. INTRODUCTION

The policies in the energy sector are an integral parts of national policies as a whole, and are closely related to the growth of the economy, population and the supply of energy.

The growth of economics, the demand for electricity continuously

grows from year to year, especially in Java and Bali areas which consumes 80% of Indonesian electricity (Bakoren, 1991). The growth is in accordance to the forecast of electricity growth in the average of 15.5% per year during the fifth Repelita (National five year development planning) and the increase to 17.7% during the sixth Repelita before it

decreases to 14.1% in the seventh Repelita.

To fulfill the growing demand of electricity and to improve the service to users, the government of Indonesia had build several steam generated electrical power plant (PLTU), one of which is "PLTU Tambak Lorok Semarang".

PLTU Tambak Lorok is a power plant which uses steam as the main force to move the turbine to create electricity. The system is functioning by using sea water as the working liquid. The clean water is turned into steam in the boiler and out from turbine, then being put into a condenser with the chillier from sea water and to turn its thermal water discharged effluent back to sea water. The residual chillier which has now become hot water is discarded through an outlet to Tanjung Emas harbor pond (Sudibyo, et al, 1993). The discarded water is called "thermal effluent" and it will cause changes in sea temperature in the surrounding areas (Burhanuddin. 1988).

In this research, the problem is emphasised on simulation of the dynamic models of thermal effluent system on the physical and chemical characteristics of sea water and aquatic biota in the waste outlet region. If the water effluent is discarded excessively so that it exceeds the tolerance of surrounding sea water body, the waste will be poisonous. It brings the declines in quality of the water in terms of physical-chemical characteristics, its, and diversity index of aquatic biota (plankton).

II. STUDY OBJECTIVE

This research intends to capture the idea or to formulate the model of water effluent effect on the physical-chemical characteristic of the water and aquatic biota in a simple way. Furthermore, this research can be used as an inputs for the policy of good management to the Steam Power Plant, so that its environmental impact can be minimised.

III. METHODOLOGY

By way of the simulation of the model, one chooses an approach with the analytical method of dynamic system which uses the program "Powersim version 2.01" copyright 1993-1995 by Modelldata, U.S.A. to know the immensity of the effects of each factor and relationship. The relationship among each interacting and affecting factors behaves differently. This shows the complexity of the water effluent model.

To validate model, one uses unit analysis, model simulation in graphics and tables and verifications. In the model simulation on parameters as the starting value one choose the standard quality value according to Kepmen KLH No.Kep.02/Men.KLH/1988 about the sea pollution for fishery. Model verification is done by measuring on the field with 2 samplings at 6 stations in the water at harbor Tanjung Emas (Table 1 and 2).

Table 1. Analysis Water Quality in the Pond of Tanjung Emas Harbor Semarang (Sampling I)

Variable	Dimen-tion	Quality in Station					
		I	II	III	IV	V	VI
1. P-total	mg/liter	0,2103	0,2125	0,0245	0,0522	0,2216	0,4873
2. N-total	mg/liter	2,0392	3,2752	1,1008	1,0962	2,2024	6,5666
3. pH	-	7,8	6,5	7,2	7,5	7,2	8,1
4. Dissolved Oxygen	mg/liter	6,0410	6,1212	5,6244	5,8854	6,0047	4,2164
5. CO2 free	mg/liter	4,2220	5,0624	4,7721	5,0243	4,2651	4,1654
6. BOD ₅	mg/liter	2,5522	3,0520	0,8000	0,8000	3,0216	3,6658
7. COD	mg/liter	5,7120	6,8000	1,1160	3,3322	5,2520	9,1262
8. Chlor free	mg/liter	17,02	16,24	22,16	13,16	14,82	14,06
9. Temperature	°C	30,7	30,7	34,3	29,4	32,4	32,6

Table 2. Analysis Water Quality in the Pond of Tanjung Emas Harbor Semarang (Sampling II)

Variable	Dimen-tion	Quality in Station					
		I	II	III	IV	V	VI
1. P-total	mg/liter	0,1976	0,2125	0,0314	0,0617	0,2664	0,5249
2. N-total	mg/liter	3,1865	3,2752	1,4266	0,9645	2,4353	6,8762
3. pH	-	7,7	6,5	7,5	7,5	7,2	7,8
4. Dissolved Oxygen	mg/liter	6,1467	6,0166	5,1422	5,3506	6,2122	5,0264
5. CO2 free	mg/liter	5,2560	5,1104	4,7428	4,4246	4,8105	5,0126
6. BOD ₅	mg/liter	2,6452	3,0520	1,2260	1,2260	3,1954	4,0124
7. COD	mg/liter	8,4216	6,8000	3,1652	3,1652	6,5524	9,7882
8. Chlor free	mg/liter	17,21	16,24	23,08	23,08	14,02	15,11
9. Temperature	°C	32	32	36,5	31	36	32

Note : Station I : East of harbor pond
 Station II : Harbor pond
 Station III : Outlet

Station IV : Mouth of outlet
 Station V : Intake
 Station VI : Near Syah-Bandar

The figuring of the causal relationship among those factors is carried out by developing a subsystem model and building it from the model's subsystems to make a big system. (Figure 1 and 2). From the assumptions in

equation taken from several simulation, the model can support the concept of water effluent pollution cycle which affects various the forming of some kind of pollution system (Appendices 1).

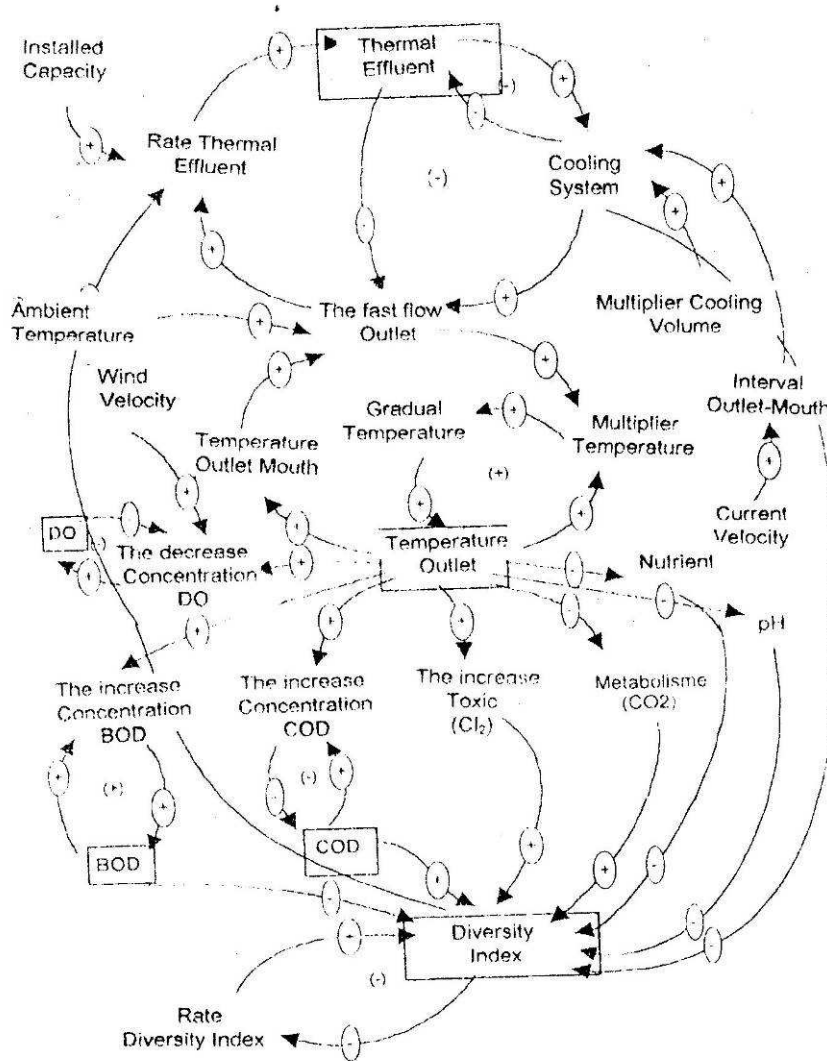


Figure 1. Causal loop diagram of thermal water discharged effluent from the steam electrical generating power plant "Tambak Lorok".

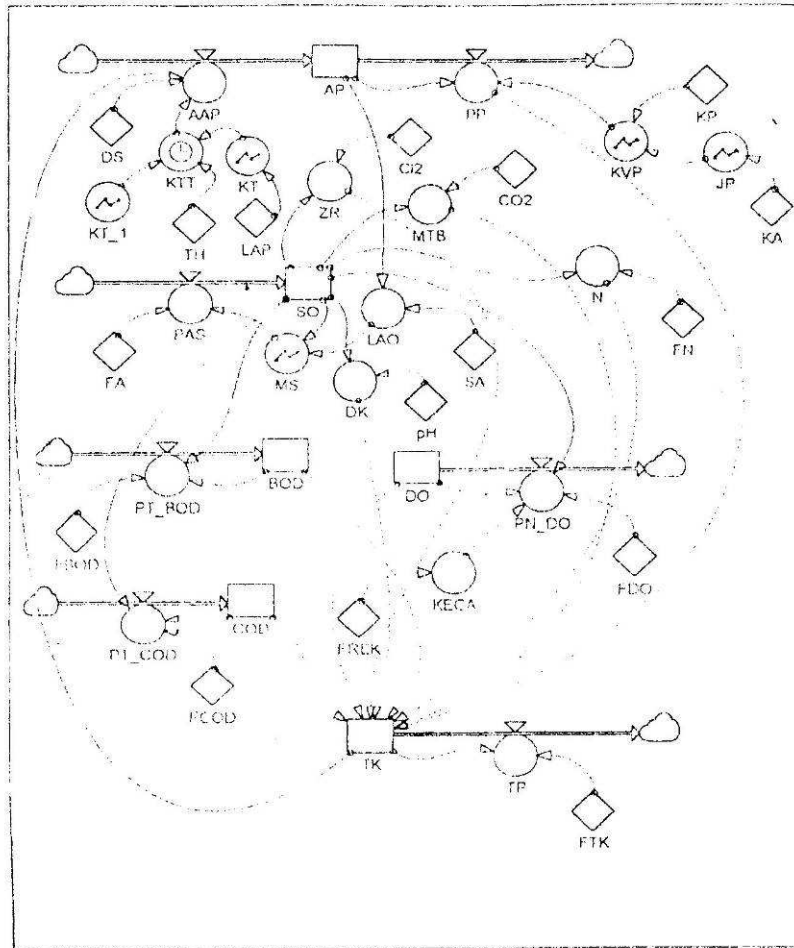


Figure 2. Flow diagram of the relationship of thermal effluent from the steam electrical generating power plant "Tambak Lorok"

IV. RESULTS AND DISCUSSION

Analysis result shows that water effluent discarded into water can change its temperature and becomes higher than the ambient level (30°C) at about 7°C. The water temperature increase affects the oxygen solvability. The higher the temperature, the lower

the oxygen solvability, so that the oxygen in the water is weak.

In the dynamic system model simulation produced will be repeated from time to time, at waste temperature equal to 37°C and solved oxygen (DO) equal to 7 mg/l, the diversity index acquired from the simulation is 2.63. It shows the polluted water condition at the middle level (Figure 3.).

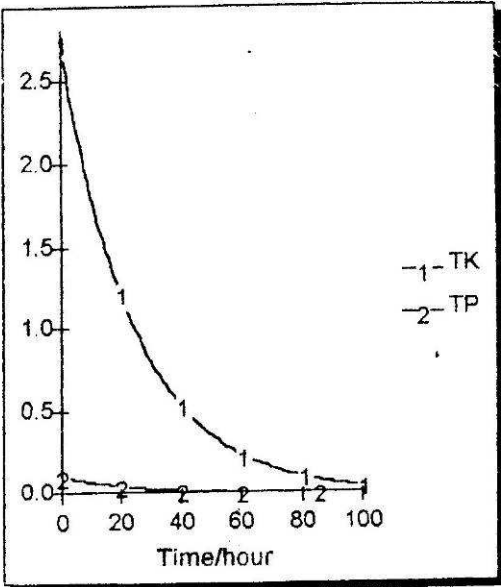


Figure 3.

Curve Diversity Index (TK) and Rate Diversity Index (TP) acquired from the simulation with time

The increase of water temperature causes solved oxygen to decrease, biology oxygen demanded (BOD) to increase, and chemical oxygen demanded (COD) to increase, too. The system of dynamic model simulation with respect to time shows that diversity index affected by information flow from DO, BOD, and COD with the existence of the cooling system is very small, close to 0 (zero). (Figure 4, 5 and Table 3).

This shows that the water biota in the outlet were all died, although when sampled, several kinds of plankton were still found. Considering that plankton is floating, the capture of the plankton may start from the outlet.

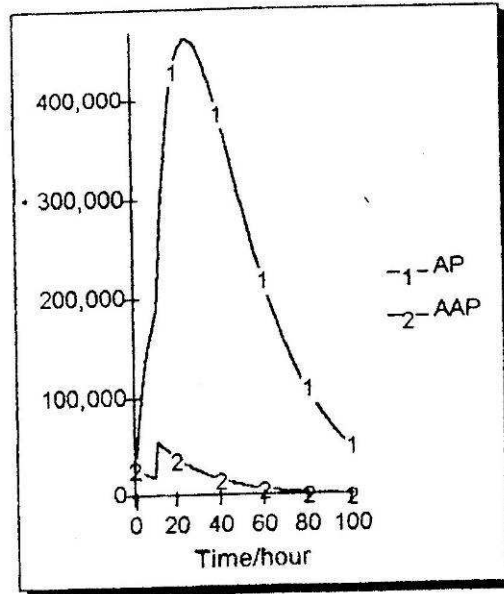


Figure 4.

Curve Thermal Effluent (AP) and Fast Flow Outlet (AAP) with time

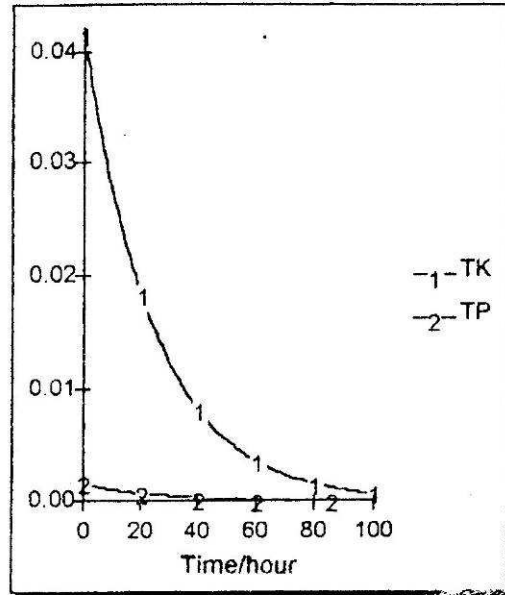


Figure 5.

Curve Diversity Index (TK) and Rate Diversity Index (TP) with ime affected by information flow from DO, BOD, and COD with the existence of the cooling system

Table 3. Thermal Effluent, Temperature, DO, BOD, COD and Diversity Index

Time	SO	DO	PN_DO	BOD	PT_BOD	COD	PT_COD	TK	TP
0	37.00	7.00	0.00118	25.00	0.0203	40.00	0.0324	2.7	0.11
1	37.00	7.00	0.00118	25.02	0.0203	40.03	0.0325	2.6	0.11
2	37.02	7.00	0.00118	25.04	0.0203	40.06	0.0325	2.5	0.10
3	37.04	7.00	0.00118	25.06	0.0203	40.10	0.0325	2.4	0.10
4	37.05	7.00	0.00118	25.08	0.0203	40.13	0.0325	2.3	0.09
5	37.07	6.99	0.00118	25.10	0.0203	40.16	0.0325	2.2	0.09
6	37.09	6.99	0.00118	25.12	0.0203	40.19	0.0325	2.1	0.09
7	37.11	6.99	0.00118	25.14	0.0203	40.23	0.0325	2.1	0.08
8	37.12	6.99	0.00118	25.16	0.0203	40.26	0.0325	2.0	0.08
9	37.14	6.99	0.00118	25.18	0.0203	40.29	0.0325	1.9	0.08
10	37.16	6.99	0.00118	25.20	0.0203	40.32	0.0326	1.8	0.07
11	37.18	6.99	0.00118	25.22	0.0204	40.36	0.0326	1.8	0.07
12	37.19	6.99	0.00117	25.24	0.0204	40.39	0.0326	1.7	0.07
13	37.21	6.98	0.00117	25.26	0.0204	40.42	0.0326	1.6	0.06
14	37.23	6.98	0.00117	25.28	0.0204	40.46	0.0326	1.5	0.06
15	37.25	6.98	0.00117	25.30	0.0204	40.49	0.0326	1.5	0.06
16	37.26	6.98	0.00117	25.33	0.0204	40.52	0.0326	1.4	0.06
17	37.28	6.98	0.00117	25.35	0.0204	40.55	0.0326	1.4	0.05
18	37.30	6.98	0.00117	25.37	0.0204	40.59	0.0326	1.3	0.05

The increasing temperature in the pond of Tanjung Emas Harbor because of water effluent, PLTU was thought the main culprit of the decrease

of number and kinds of planks in the water. The diversity index measured in the outlet are 1.43 and 1.44 (Table 4 and 5).

Table 4. Kinds of Plankton in the Observed Stations (Sampling I)

No	Organisme	Total Individu per liter					
		I	II	III	IV	V	VI
1.	<i>Skeletonema sp.</i>	32	29	11	20	6	8
2.	<i>Nitzschia sp.</i>	14	14	3	6	30	9
3.	<i>Chaetoceros sp.</i>	8	8	-	5	5	4
4.	<i>Pleurosigma sp.</i>	8	8	-	-	-	-
5.	<i>Rhizosolenia sp.</i>	7	8	-	4	3	6
6.	<i>Oscillatoria sp.</i>	7	7	-	2	2	-
7.	<i>Surirella sp.</i>	6	6	-	-	1	-
8.	<i>Ceratium sp.</i>	6	5	-	1	2	5
9.	<i>Thalassiothrix sp.</i>	3	4	-	-	-	1
10.	<i>Asterionella sp.</i>	3	-	-	-	-	-
11.	<i>Peridinium sp.</i>	2	3	-	-	-	-
12.	<i>Cyclops sp.</i>	2	2	-	-	-	-
13.	<i>Dunaliella sp.</i>	-	-	2	-	-	-
14.	<i>Ulothrix sp.</i>	-	-	1	-	-	-
15.	<i>Chlorella sp.</i>	-	-	1	-	-	-
16.	<i>Melosera sp.</i>	-	-	1	-	-	-
17.	<i>Lauderia sp.</i>	-	-	-	1	1	1
18.	<i>Rhopaloidea sp.</i>	-	-	-	-	1	-
19.	<i>Hemidiscus sp.</i>	-	-	-	-	1	-
Kinds Total (t)		12	11	7	8	10	7
Total Individu (N)		98	94	20	44	52	35
Diversity Index (H')		2,12	2,10	1,43	1,58	1,49	1,77
Average Index (J)		0,85	0,87	0,73	0,75	0,64	0,90

Table 5. Kinds of Plankton in the Observed Stations (Sampling II)

No	Organisme	Total Individu per liter					
		I	II	III	IV	V	VI
1.	<i>Skeletonema sp.</i>	33	30	10	19	6	9
2.	<i>Nitzschia sp.</i>	18	16	2	6	28	9
3.	<i>Chaetoceros sp.</i>	9	9	-	4	5	4
4.	<i>Pleurosigma sp.</i>	9	7	-	-	-	-
5.	<i>Rhizosolenia sp.</i>	8	8	-	2	3	5
6.	<i>Oscillatoria sp.</i>	7	6	-	1	2	-
7.	<i>Surirella sp.</i>	7	-	-	-	1	-
8.	<i>Ceratium sp.</i>	7	4	-	-	1	2
9.	<i>Thalassiothrix sp.</i>	5	3	-	-	-	1
10.	<i>Asterionella sp.</i>	6	5	-	-	-	1
11.	<i>Peridinium sp.</i>	3	2	-	1	-	-
12.	<i>Cyclops sp.</i>	2	-	-	-	-	-
13.	<i>Dunaliella sp.</i>	-	-	2	-	-	-
14.	<i>Ulothrix sp.</i>	-	-	1	3	-	-
15.	<i>Chlorella sp.</i>	-	-	1	3	-	-
16.	<i>Melosera sp.</i>	-	-	-	-	-	-
17.	<i>Lauderia sp.</i>	-	7	1	4	3	5
18.	<i>Rhopaloidea sp.</i>	-	-	-	-	1	-
19.	<i>Hemidiscus sp.</i>	-	-	-	-	1	-
20.	<i>Euchampia sp.</i>	-	-	1	-	-	-
Kinds Total (t)		12	11	7	9	10	8
Total Individu (N)		114	97	18	43	51	36
Deversity Index (H')		2,20	2,25	1,44	1,75	1,55	1,83
Average Index (J)		0,88	0,96	0,74	0,80	0,67	0,88

Note : Station I : East of harbor pond
 Station II : Harbor pond
 Station III : Outlet

Station IV : Mouth of outlet
 Station V : Intake
 Station VI : Near Syah-Bandar

There were two kinds of plankton found in all the observation stations, namely Skeletonema and Nitzschia which can survive at 37°C. The dynamic system model simulation showed that the temperature effect on DO, BOD, COD, Cl₂, CO₂, nitrogen and pH will improve the water condition with diversity index equal to 1.57, and will decrease according to the temperature condition with respect to time (Figure 6).

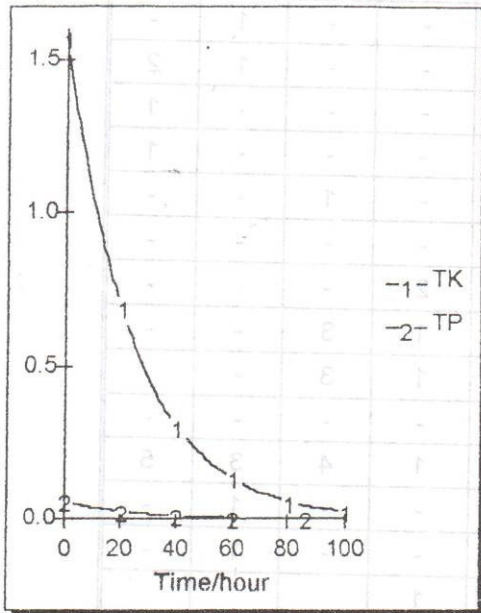


Figure 6.

Curve Diversity Index (TK) and Rate Diversity Index (TP) versus time with that the temperature effect on DO, BOD, COD, Cl₂, CO₂, nitrogen and pH

Increasing the installed capacity to 500 MW causes the water effluent debit to increase 250% which accelerates the increase of water temperature. The increase temperature by 2°C, means that the temperature will be

39°C. This condition causes a re-circulation to the intake. The system of dynamic simulation model shows that the heat increase from the water effluent was faster than before the installed capacity had been increased. In the mean time, the hot water flow shows the stability or "goal seeking" for a relatively long time (Figure 7).

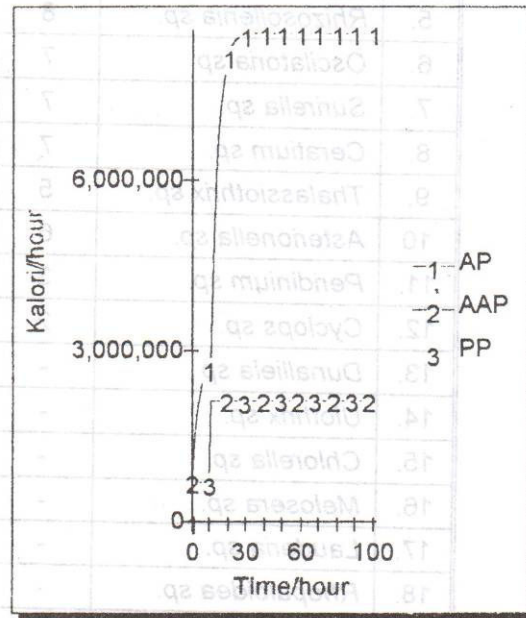


Figure 7.

Curve Thermal Effluent (AP), Fast Flow (AAP) and Cooling System (PP) with time

To maintain a good water condition, the policy taken should be by disconnecting the heat flow (material flow) in the model, which means the water effluent is not discarded in the outlet as is the case in the current situation. The flow disconnection means moving the outlet or the waste channel. Even, according to the result of study conducted together by PLN and UGM, to stop

the re-circulation to the intake, the water effluent channel is to be moved to east of the harbor pond. From the natural environment, this is very beneficial because the water effluent will immediately be thinned out by the atmosphere, so that the value of diversity index shows an unpolluted water condition.

V. CONCLUSIONS

The increase of water temperature causes oxygen to decrease, biology oxygen demanded (BOD) to increase, and chemical oxygen demanded (COD) to increase. The system of dynamic model simulation with respect to time shows that diversity index affected by information flow from DO, BOD and COD with the existence of cooling system is very small.

With the increase of temperature in the pond of Tanjung Emas Harbor caused by water effluent, PLTU was thought to be the main culprit of the decrease of numbers and kinds of plankton in the water. There are two kinds of plankton found in all the observation stations, namely *Skeletonema* and *Nitzschia* which survive at 37°C.

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Appendices 1.

init	AP = 0	N = SORFN	aux
flow	AP = -dt*PP	N = Nitrogen	doc
	+dt*AAP	ZR = SORCIS	aux
doc	AP = Thermal Effluent	CIS = Free chlorine	doc
init	BOD = 25	CO2 = 12	aux
flow	BOD = +dt*PT_BOD	Carbon Dioxide	doc
doc	BOD = Biology Oxygen Demand	DS = 8	const
init	COD = 40	DS = Delta temperature	doc
flow	COD = +dt*PT_COD	FA = Fraction hot flow	const
doc	COD = Chemical Oxygen Demand	FBOD = 0.03	aux
init	DO = 7.8	FBOD = Fraction BOD	doc
flow	DO = -dt*PN_DO	FCOD = Fraction COD	aux
doc	DO = Dissolve Oxygen	FDO = 0.03	const
init	SO = 30	FDO = Fraction DO	doc
flow	+dt*PAS	FN = 1	const
doc	SO = Temperature outlet	FN = Fraction Nitrogen	doc
init	TK = 300/(BOD+COD+DO)+PP	FREK = 0.04	const
flow	TK = -dt*TP	FREK = Fraction diversity index	doc
doc	TK = Diversity index	KA = 43.2	const
aux	AAP = (KTT*DS*1020*0.998)*TK	KA = Current velocity	doc
doc	AAP = The hot water flow	KP = 0.25	const
aux	PAS = MS*FA	KP = Cooling system	doc
doc	PAS = Temperature outlet flow	LAP = 192.8	const
aux	PN_DO = (DO/SO)*FDO*KECA	LAP = Rate hot water WWM	doc
doc	PN_DO = The decrease of DO	SA = 30	const
aux	PP = AP/KVP	SA = Ambient temperature	doc
aux	PT_BOD = (BOD/SO)*FBOD	TH = 1997	const
doc	PT_BOD = The increase of BOD	TH = The year increasing the installed capacity	doc
aux	PT_COD = (COD/SO)*FCOD		
doc	PT_COD = Fraction COD		
aux	TP = TK*FTK		
doc	TP = The decrease of diversity index		
aux	JP = GRAPH(KA,0,100,[100,200,300,400,500,600,700,800"Min:0;Max:800"])		
doc	JP = Gradual temperature		
aux	KECA = 1.39*FREK		
doc	KECA = Wind velocity		
aux	KT = GRAPH(LAP*TIME,1978,2(100,100,100,300,300,300,300,300,300))		
doc	KT = The installed capacity		
aux	KT_1 = GRAPH(TIME,1997,2[500,500,500])		
doc	KT_1 = Increasing the installed capacity		
aux	KTT = IF(TIME>=TH,KT,KT_1)		
doc	KTT = Addition the installed capacity		
aux	KVP = GRAPH(JP*KP,0,2[3,5,7,9,11,13,15"Min:0;Max:20"])		
doc	KVP = Multiplier volume		
aux	LAO = SA		
aux	MS = GRAPH(SO/LAO,0,1,[7,6,5,4,3,2,1"Min:0;Max:7"])		
doc	MS = Multiplier temperature		
aux	MTB = SO/CO2		
doc	MTB = Metabolisme		

aux	N = SO/FN	AP = 70	init
doc	N = Nitrogen	AP = -dl*PP	flow
aux	ZR = SO/CI2	+dl*AP	doc
const	CI2 = 0.5	AP = Thermal Effluent	doc
doc	CI2 = Free chlorine	BOD = 25	init
aux	CO2 = 12	BOD = +dl*PT_BOD	flow
doc	Carbon Dioksida	BOD = Biology Oxygen Demand	doc
const	DS = 9	COD = 40	init
doc	DS = Delta temperature	COD = +dl*PT_COD	flow
const	FA = Fraction hot flow	COD = Chemical Oxygen Demand	doc
aux	FBOD = 0.03	DO = 7.8	init
doc	FBOD = Fraction BOD	DO = -dl*PN_DO	flow
aux	FCOD = Fraction COD	DO = Dissolve Oxygen	doc
const	FDO = 0.03	SO = 30	init
doc	FDO = Fraction DO	+dl*PAS	flow
const	FN = 1	SO = Temperature outlet	doc
doc	FN = Fraction Nitrogen	TK = 300(BOD+COD+DO)+PP	init
const	FREK = 0.04	TK = -dl*TP	flow
doc	FREK = Fraction diversity index	TK = Diversity index	doc
const	KA = 43.2	AAP = (KTT*DS*1020*0.898)*TK	aux
doc	KA = Current velocity	AAP = The hot water flow	doc
const	KP = 0.25	PAS = MS*FA	aux
doc	KP = Cooling system	PAS = Temperature outlet flow	doc
const	LAP = 193.5	PN_DO = (DO/50)*FDO*KECA	aux
doc	LAP = Rate hot water MW/hour	PN_DO = The decrease of DO	doc
const	SA = 30	PP = AP/KVP	aux
doc	SA = Ambient temperatur	PT_BOD = (BOD/50)*FBO	aux
const	TH = 1997	PT_BOD = The increase of BOD	doc
doc	TH = The year increasing the installed capacity	PT_COD = (COD/50)*FCOD	aux
		PT_COD = Fraction COD	doc
		TP = TK*TK	aux
		TP = The decrease of diversity index	doc
		JP = GRAPH(KA,0,100,100,200,300,400,500,600,700,800,Min,0,Max,800)	aux
		JP = Gravel temperature	doc
		KECA = 1.39*FREK	aux
		KECA = Wind velocity	doc
		KT = GRAPH(LAP*TIME,1978,2100,100,100,200,300,300,300)	aux
		KT = The installed capacity	doc
		KT_1 = GRAPH(TIME,1997,21500,500,500)	aux
		KT_1 = increasing the installed capacity	doc
		KTT = IF(TIME>TH,KT,KT_1)	aux
		KTT = Addition the installed capacity	doc
		KVP = GRAPH(JP*KP,0,213,5,7,9,11,13,15,Min,0,Max,20)	aux
		KVP = Multiplier volume	doc
		LAO = SA	aux
		MS = GRAPH(SO,LAO,0,1,7,8,5,4,3,2,1,Min,0,Max,7)	aux
		MS = Multiplier temperature	doc
		MTB = SO/CO2	aux
		MTB = Metabolisme	doc