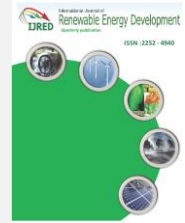




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Kinetic and Enhancement of Biogas Production for The Purpose of Renewable Fuel Generation by Co-digestion of Cow Manure and Corn Straw in A Pilot Scale CSTR System

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ABSTRACT. Biogas production from anaerobic co-digestion of cow manure (CM) and corn straw residue (CSR) were experimentally investigated using a completely stirred tank reactor (CSTR) under semi-continuously feeding circumstance at mesophilic (35°C±2) temperature. The pilot-scale digester with 180 L in volume was employed under experimental protocol to examine the effect of the change in organic loading rate on efficiency of biogas production and to report on its steady-state performance. An average organic loading rates of 2 and 3 kg VS. (m⁻³.d⁻¹) and a hydraulic retention time (HRT) of 25 days was examined with respect to two different CM to CSR mixing ratios of 100:0, 75:25 and 50:50, respectively. The results showed both organic loading rates at co-digestion of CM+ CSR gave better methane yields than single digestion of cow manure. The biogas production efficiency was obtained 0.242, 0.204, 0.311 0.296, 259.5 and 235 m³.(kg VS input)⁻¹ for 2 and 3 kg VS.(m⁻³.d⁻¹) at CM to CSR mixing ratios of 100:0, 75:25 and 50:50, respectively. The reactor showed stable performance with VS reduction between 55-74% during different runs. With increment of loading rate, the VS degradation and biogas yield decreased. Modified Gompertz and logistic plot equation was employed to model the methane production at different organic loading rates and substrate concentrations. The equations gave a good approximation of the maximum methane production (r_m) and the methane yield potential (P) with correlation coefficient (R²) over 0.99.

Keywords: Biogas; cow manure; corn straw; Kinetic; semi-continuously

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1. Introduction

One of the renewable energy sources is biogas for fossil fuel, which is made from innocuous, safe and biodegradable in the environment such as municipal waste, industrial waste and agricultural, animal and domestic wastes (Omer *et al.*, 2002). Anaerobic digestion (AD) is decomposition of organic matter such as manure, crop residues in the absence of oxygen by concerted action of different groups of anaerobic bacteria. The AD process that is an important energy source produces biogas that the main component composed of methane (CH₄), and carbon dioxide (CO₂) which can be consumed as an energy source. Biogas can be directly burned in a combined and heat power unit for the generation of heat and electricity (Ray *et al.*, 2016; Song *et al.*, 2012).

Biogas produced from biogenic material, the feedstock used for biogas production constitute of mono substrate or co-digestion of mixture of several organic materials depending on the reactor technology, availability of feedstock, economic consideration etc., is a type of biofuel (Themelis, & Ulloa, 2007). AD of organic materials to biogas is characterized by the four major steps: hydrolysis, acidogenesis, acetogenesis and methanogenesis consecutively. All the mentioned steps run almost at the same time in a biogas reactor. Nearly seventy percent of methane from biogas reactors fed with cattle manure is derived from acetate (Umar *et al.*, 2013; Zhang & Zhang, 1999). The quantity and quality of biogas depend on characteristics of feedstock as well as process conditions.

Anaerobic fermentation of animal slurry for biogas generation is commonly tested in continuously stirred

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tank reactor (CSTR) and sporadically in plug-flow reactor (Wilkie & Evans, 2010). In a biogas process with a typical hydraulic retention time (HRT) of 15–30 days, 50–70% of organic matter is transformed into biogas with an average methane yield of 0.20–0.25 m³ per kg of added volatile solids (Hartmann *et al.*, 2003). In a study, Boe (2006) indicated that serial digestion, with volume distributions ratio of 90:10 or 80:20 between the two methanogenesis reactors, improved biogas production by 11% compared to an ordinary one-step CSTR process. In addition, modeling results from this study established that the longer of hydraulic retention time in the post-reactor (second digester of serial process), the higher the methane production of the overall serial digestion (Boe, & Batstone, 2005).

Agricultural segment provides numerous biomass residues, and it has diversely been estimated that these wasted materials can account for over 30% of global agricultural productivity (Oliveira, & Franca, 2009). Corn straw residues that are produced from this part, containing husk, stover, and cob, are lignocellulosic biomass that has been commonly used as one of the conventional substrates for biogas production plants. With the high content of cellulose and hemicelluloses, corn straw residues are considered to be a suitable feedstock for the biogas production. Lignocelluloses are mainly consisting of cellulose, hemicelluloses, lignin, and extractives (Karimi *et al.*, 2013). Mixing organic matters by two or further substrates, which is commonly known as co-digestion, may give a synergistic result that can effect in the higher biogas production (Deublein & Steinhauser, 2011).

This operation amends the biogas efficiency and methane content in during digestion process and heavily dependent on the organic loading rate (OLR) of co-substrates to the fermentation process. The most popular utilization of co-digestion can be established in agricultural biogas plants by application a fundamental substrate such as animal manure and by adding a little amount of extra substrates (Pesta, 2007). Furthermore, in anaerobic fermentation process, the organic loading rate (OLR) is a main parameter because it illustrates the amount of volatile solids to be fed into the reactor each day (Mattocks, 1984). Other OLR affects the stability of the anaerobic digestion process and biogas production rate by preparing digestible substrates for the population growth of microorganisms (Taricska *et al.*, 2009). Volatile solids indicate that portion of the organic-material solids that can be digested, while the remaining of the solids is fixed. The actual loading rate depends on the kinds of wastes fed into the reactor (Pesta, 2007). Thus, it is a main parameter implying how much organic dry matter (DM) can be fed in reactor per unit of volume and time, and relates to the time that the biomass is retained within the reactor (Lichtman, 1983). Increase in biogas or methane production has been reported from co-digesting cow manure or animal wastes with crop residues since

wheat straw, rice straw, sugarcane stalk, maize stalks, cotton stalks, onion waste, Potato Pulp and oil palm fronds (Somayaji & Khanna, 1994; Sharma, 2002; Karellas *et al.*, 2010; Tong *et al.*, 2013; Sanaei-Moghadam *et al.*, 2014; Zhang, *et al.*, 2014).

The lignocellulosic of biomass is rich in carbon, and thus it is important that such material be co-digested simultaneously with materials rich in nitrogen in order to obtain a suitable balance of nutrient, good efficiency, and stability in an anaerobic digester (Jagadabhi *et al.*, 2008 ; Deublein & Steinhauser, 2011). In a previous study consisted of batch assays, co-digestion of steam-exploded Salix and manure led to steady state methane production and more upper compared to single reactor of those substrates. Maximum methane production were produced at C/N ratios of 35-40, which corresponded to about 30-40% VS from Salix in the co-digestion (Estevez *et al.*, 2012).

Many researchers have studied the reaction kinetics of biogas production and developed kinetic models for evaluating the anaerobic digestion process (Zhu *et al.*, 2009; Maamri & Amrani, 2014; Latinwo & Agarry, 2015). Moreover, cumulating of biogas could be simulated by logistic and modified Gompertz as well as exponential rise to maximum equations which were universally employed for the simulation of biogas, methane and hydrogen production (Wang & Wan 2009; Altas, 2009). For example Lo and co-workers reported that the biogas production rates of municipal solid waste (MSW) were increased by applying suitable dose of fly ashes (FA/MSW =20 and 10 g.L⁻¹) and bottom ashes (BA/MSW=100 g.L⁻¹) compared to control. Equation of modified Gompertz indicates higher correlation of biogas and methane accumulation than exponential rise to maximum model for every digesters (Lo *et al.*, 2010).

The objective of this study was to determine the effect of OLRs and substrate mixing ratio as co-digested in the form of cow manure/corn straw residue as well as acquiring kinetic models for biogas production by a completely stirred tank reactor (CSTR) under semi-continuous feeding in pilot scale at mesophilic conditions. In addition, specific cumulative biogas production was simulated using exponential rise to maximum, logistic growth model and modified Gompertz models, respectively.

2. Materials and Methods

2.1. Substrates and Inoculum

The study was performed in 2015-2016 at the Agricultural research center of Ardabil Province, Moghan (39.39 °N, 48.88° E) in the Northwestern part of Iran. The mean annual precipitation and temperature at the station are 332 mm and 21.5°C, respectively. Fresh cow manure was obtained from the Cow Unit in cow development department in Animal Breeding and Animal Husbandry, Moghan. It was kept in 30 L

containers at ambient temperature until fed to the reactors. Corn straw residue was collected from Corn Farm in Agriculture Research Centre of Ardabil, Iran and was chopped on site. The precision-chop CSR had an average size of 1-2 cm and was stored in ambient temperature. The inoculum used in the current reactors originated from an existing demonstration digester at Materials and Energy Research Center, Karaj, Iran in which the gas potential of different mixtures of pre-treated cattle manure was evaluated. The digested material from the earlier experiment was pooled in a container and maintained anaerobically for one week at 35°C before being used as inoculum in the CSTR system. The characteristics of fresh cow manure, corn straw residue and inoculum are given in Table 1.

Table 1
Characteristics of inoculum, cow manure and corn straw residue

Parameters	Inoculum	Cow manure	Corn straw
TS(%)	7.11 (%FM)	(%FM) 16.21	90.4
VS(%)	5.50 (%TS)	(%FM) 13.48	88.3
VS: TS(%)	77.38	83.41	97.67
pH	7.08	7.49	N.D
EC (ms/cm)	17.05	9.81	N.D
TC(%)	37.15 (%TS)	32.40 (%TS)	43.90
TN(%)	1.74 (%TS)	1.98 (%TS)	0.63
C/ N	21.35	16.36	69.68

TS: total solid, VS: volatile solids, TC: Total carbon; TN: total nitrogen, FM: Fresh matter, DM: Dry matter; and ND: Not determined

2.2. Experimental setup and operation

A CSTR pilot-scale digester was designed with the purposes of ease of transportation of the digester to the site and automatic operation and control. The digester tank was cylindrical in shape with 110 cm height and 46 cm diameter, made from 4 mm thickness galvanized steel sheet. Its capacity was 180 l, with 140 L working volume as shown in Fig.1. The system can be divided into four sectors: control panel, feeding system, digester and agitation system and gas metering device. The digester was fitted with an adequate top plate, which

supported the mixer, mixer motor (electrical three-phase 380 V machine coupled with 15:1 gearbox), gas measurement and sampler. Sampling valves were located at relevant positions for gas and digester contents. The feeding system is at the top of the reactor. It has one outlet at the bottom for effluent discharge. Other tools and devices were used for biogas measurement and storage system consists of biogas piping, a biogas flow meter (displacement water), a biogas bag (tube), jackets, thermometer, pH sensor with conductivity measuring probe, circulating substrate through the reactor by mechanical stirrer (two propellers), control-bar and timer for timing the operation. The experiment was operated in semi-continuous mode with daily feeding. Semi-continuous anaerobic digestion of cow slurry and corn straw residue was investigated in mesophilic condition (35°C±2) with three different organic loading rates (OLR) of 1.4, 2 and 2.75 kg VS/(m³.d) for constant retention time of 25 days.

The experiment was run at mesophilic condition (35°C±2) using cow manure and corn straw residue in pilot-scale of AD and HRT equal to 25 days. This was done by placing a mixture of substrates in a floating drum container that was run with respect to two different cow manure (CM) to corn straw residue (CSR) mixing ratios of 100:0, 75:25 and 50:50, to the semi-continuously fed tank reactor which employed with two different organic loading rates (OLR) of 2 and 3 kg VS. (m⁻³.d⁻¹), respectively. Retention time of 25 days was maintained by feeding 5.6 L of substrate and removing 5.6 L of effluent daily and mixed slowly for 15 min every 45 minutes at a speed of about 100 rpm according to Adebayo et al, (2015). The CSTR digester was filled with 60 liters of seed sludge (inoculum) for startup and addition of substrate was started with 80 liters using only cow slurry at 2 kg VS. (m⁻³.d⁻¹) OLR.

The start-up period lasted one week and normal operation of the reactor continued afterwards on one daily feeding, 7 days a week, at a defined OLR and retention time of 25 days. Thus, 5600 mL of freshly prepared substrate mixture was added to digester and then an equivalent volume was discharged, so to maintain the volume inside the reactor constant.

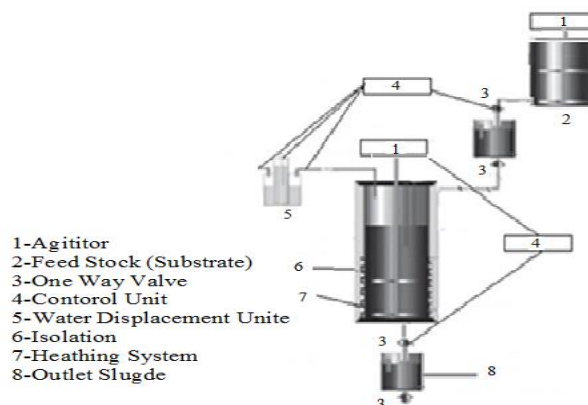


Figure 1. Schematic of digine semi- continues digester and elements

To evaluate the effects of co-digestion, the experimental run C was fed with a mixture of 75% CM and 25% CSR (VS-basis) quantity and the substrate mixture was diluted with water to achieve an initial OLR of 2 kg VS (m⁻¹.d⁻¹). Experimental run D was used to the same mixture as run C but with OLR= 3kg VS.(m⁻¹.d⁻¹) and run E and F were fed with a mixture of 50% CM and 50% CSR (VS-basis) quantity. The substrate mixture was diluted with water to achieve an initial OLR of 2 and 3 kg VS(m⁻¹.d⁻¹), whereas run A and B were fed solely with cow manure at 2 and 3kg VS.(m⁻¹.d⁻¹) OLR, respectively. The details of feeding scheme are given in Table 2.

Table 2
Feeding schemes for the four runs

Run	Feedstock mixture		C/N of feedstock	OLR kg VS.(m ⁻¹ .d ⁻¹)
	Cow manure (% VS)	Corn straw (% VS)		
A	100	0	16.35	2
B	100	0	15.81	3
C	75	25	22.07	2
D	75	25	21.61	3
E	50	50	26.34	2
F	50	50	27.11	3

2.3. Basic process parameters and analytical methods

The volume of biogas was recorded by water displacement method in daily. The volume of the biogas was normalized to standard temperature and pressure. The biogas vented from the biogas piping was collected in a biogas bag for two week, all the biogas was transferred into gas chromatograph for measuring the composition of biogas (CH₄ and CO₂) (Li *et al.*, 2014). The analytical methods for total solids (TS), volatile solids (VS), pH and EC was analyzed according to the APHA standard methods and Total nitrogen (TN) estimated by the Kjeldahl method (APHA, 1998).

2.4. Methane production simulation

Cumulative methane production from the AD of the substrates was simulated using Gompertz equation, Exponential rise to maximum and Logistic equation. In addition, specific cumulative biogas or methane production was simulated using modified logistic kinetic model, exponential rise to maximum and modified Gompertz kinetic model. Exponential rise to maximum equation shown in Eq. (1) based on (Bilgili *et al.*, 2009; Zwietering, *et al.*, 1990; Lo, *et al.*, 2010)

$$Y = P(1 - \exp(-kt)) \quad (1)$$

Where Y is the cumulative methane yield (L.kg⁻¹), P is the ultimate potential of biogas or methane

production (L kg⁻¹), t is time (day) in all digestion period and k is the first order kinetic constant (d⁻¹).

The lag phase (λ) can be calculated with the modified Logistic and Gompertz model as described by Zwietering *et al.* 1990, as follows: The modified equation for simulation is a form of the Logistic equation which is generally applied to simulate the cumulative biogas or methane production is presented in Eq. (2) (Zwietering, *et al.*, 1990).

$$Y = P \left\{ 1 - \exp \left[4r_m P^{-1} (\lambda - t) + 2 \right] \right\} \quad (2)$$

For the modified Gompertz kinetic model equation is a form of the Gompertz model which is generally applied to simulate the cumulative biogas or methane production as follow Eq. (3) (Zwietering, *et al.*, 1990; Lo, *et al.*, 2010 ; Maamri & Amrani, 2014; Latinwo & Agarry, 2015).

$$Y = P \exp \left\{ - \exp \left[r_m P^{-1} e (\lambda - t) + 1 \right] \right\} \quad (3)$$

Where Y, t and P are the same as aforementioned, r_m is the maximal biogas production rate (L.kg⁻¹ d⁻¹) while λ is the lag phase (day) and e is equal to 2.718282. All regression equations were completed by MATLAB11b version.

3. Results and Discussion

3.1. Biogas and methane production

Daily biogas production rate and cumulative biogas volume from single digestion of cow manure (experimental runs A and B) and co-digestion of CM and CSR (runs C, D, E and F) are presented in Fig.2 and Fig.3. It could be seen from Fig. 2 that run A (single digestion of CM at OLR= 2) and run D (75% CM + 25% CSR (VS basis) with OLR=3) showed the lowest and highest daily biogas production respectively.

The digestion runs started the generation of biogas on the 2nd, 2nd, 3rd, 4rd, 4nd and 3rd day of feeding start, respectively. This observation indicates that biogas production started early for runs A and B and thus a reduction in start-up time as compared to co-digestions. However, the delays in biogas production may probably be due to two factors. First, the types of feeding that have been given to the cows, which are mainly agricultural crops, such as corn straw residue. Generally, about 90% of the dry weight of most plant materials is due to cellulose, hemicellulose and lignin. The existence of lignin in lignocelluloses makes a protective barrier that stops plant cell destruction by microorganisms for conversion to energy (methane content) unless of course pretreated (Avicenna, *etal.*,

2015). Different pretreatment methods can improve the physical and chemical structure within the lignocellulosic biomass and facilitates hydrolysis rates for conversion to biogas. Second, it might be as a result of volatile fatty acids (VFAs) accumulation due to the low biodegradability of cow manure, which resulted in partial inhibition in the digester. When the VFAs were consumed, the partial inhibition was overcome and biogas production started (Angelidaki, & Ahring, 1993; Avicenna et al 2015) As biogas started its generation, the results demonstrate high biogas production rates for the initial days. Another probable description for this outcome is that most of the exposed cellulose and hemicelluloses content of the substrate was degraded which make it accessible to the microorganisms for conversion to biogas.

In this study, the maximum cumulative biogas yield at day 42 was 997, 1168, 1311 and 1429 L for runs A to D, respectively. The biogas yields from co-digestion of CM and CS were significantly higher than that of single digestion of CM in both OLRs. The daily biogas rates were 7.33 and 6.39 L/ kg VS at steady state (15-35) days for single CM and 10.32 and 8.16 L/ kg VS at and 8.46 and 7.15 L/ kg VS for co-digestion of CSR/CM (50:50), in steady state (15-35) days for co-digestion of CS/CM, corresponding to OLRs equal to 2 and 3 kgVS. (m⁻³.d⁻¹), respectively (Figure 2).

Comino et al. also outstanding the effect of anaerobic co-digestion during the fermentation process of agricultural wastes. They stated the interests of optimizing the ratio of crops and organic loading rate(OLR) in co-digestion of cattle manure with energy crops by the fact that during feeding within 70% VS of crop in the feedstock, up to 109% higher specific methane yield was achieved than during the start-up run of single manure digestion (Comino *et al.*, 2013). It was also found that biogas production from cattle manure or animal wastes increases by co-digesting with crop residues like wheat straw, sugarcane stalks, maize stalks, rice straw, cotton stalks, oil palm and onion waste fronds (Somayaji & Khanna, 1994; Sharma, 2002; Karellas et al., 2010; Tong et al., 2013; Sanaei-Moghadam et al., 2014; Zhang, *et al.*, 2014).

The observed phenomenon could be attributed to additional nutrients availability (feedstock composition) and improved carbon-to-nitrogen ratio (C: N) provided by the corn straw residue. Similar observations have also been reported by Tong et al (2013), Sanaei- Moghadam et al (2014) and Latinwo & Agarry (2015). Both organic loading rates on co-digestion of CM and CSR gave better methane yields than single digestion of cow manure (Table 3). The reactor showed average biogas production efficiency was obtained 0.242, 0.204, 0.311, 0.296, 259.5 and 235m³.(kg VS input)⁻¹ for 2 and 3 kg VS.(m⁻³.d⁻¹) at CM to CSR mixing ratios of 100:0, 75:25 and 50:50, respectively.

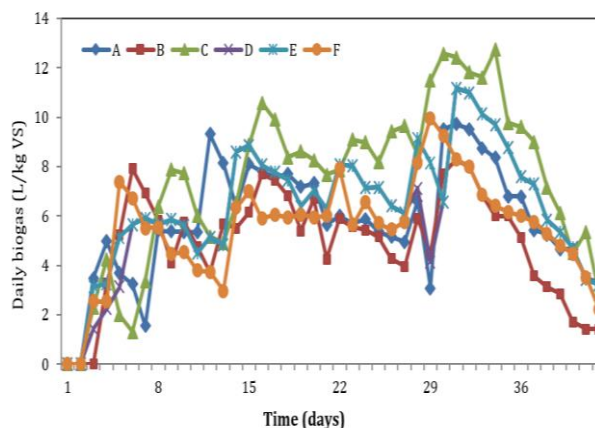


Fig. 2 The daily production rates of biogas in different runs

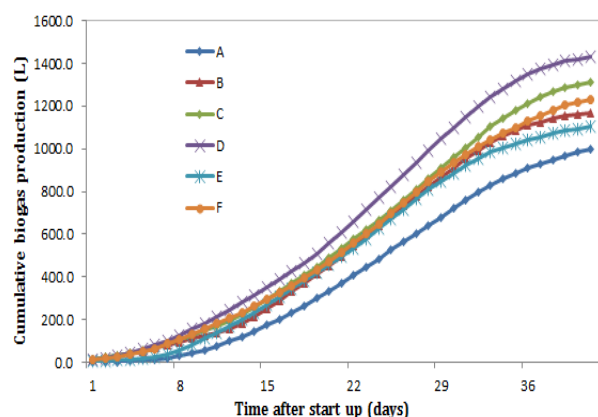


Figure 3 The cumulative biogas yields of OLR and different ratio of cow manure and co-digested with corn straw residue in different runs

In addition, VS reduction upon stable performance as 64.57, 54.96, 74.11 , 62.76 , 64.11 and 58.30% during the runs A to F, respectively. On the other hand, this study suggests that co-digestion (in runs C to F) can improve the efficiency of biogas production by about 25% comparing single digestion of cow manure (runs A and B). However, the cumulative biogas production started to decrease after 32th day in all digesters. The reactor showed stable performance with approvable methane content 54-63 percent (Table 3).

Table 3 Operational conditions for the varies runs

Run	Average methane Content (%)	Max. specific methane yield (mL g ⁻¹) ^a	Average VS reduction (%)
A	61.17	148.03	64.57
B	62.58	127.66	54.96
C	57.87	179.97	74.11
D	54.8	156.28	62.76
E	55.66	147.05	64.11
F	55.75	131.22	58.30

^a Based on weekly average production

3.2 pH profiles

In anaerobic fermentation, the bacteria of methanogenic are more sensitive than bacteria of hydrolytic and acidogenic to environmental conditions. At ambient temperature, the pH is the one of the most influential parameters that affects anaerobic digestion process (Rabah *et al.*, 2010). For instance, the pH of reactor liquid effluent showed the process stability and its variety also depends on the buffering capacity of the system (Mata-Alvarez *et al* 2000). Furthermore, it was observed that pH of the fermentation slurry was slightly dropped with increase in OLR upon single digestion of cow manure while it was maintained pretty constant against OLR increase at co-digestion runs as shown in Table 3.

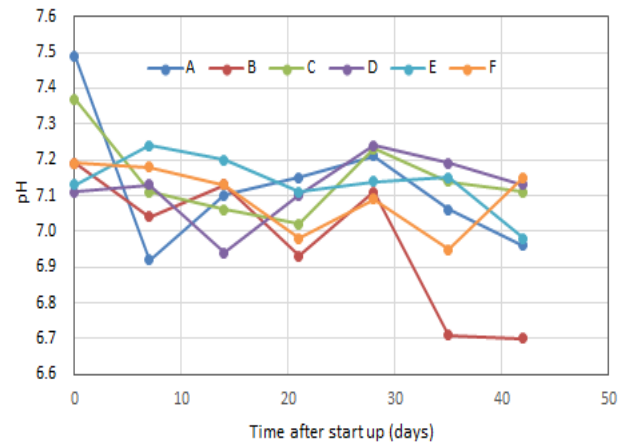


Fig. 4. pH variations of digester content during the different runs

Table 4.

Comparison of values of model constants, RMSE and coefficient of determination (R^2) obtained from kinetic models fitted to specific cumulative biogas production data in varies runs

Kinetics models	Coefficient and parameters	A	B	C	D	E	F
Modified Logistic	R^2	0.990	0.9895	0.9954	0.9924	0.9942	0.9905
	RMSE	6.120	6.912	6.997	8.139	6.108	7.146
	$P(Nl. (kg VS)^{-1})$	263.1	223.2	360.4	345.8	275.9	273.4
	$r_m(Nl. (kg VS. day)^{-1})$	8.271	6.664	10.53	8.981	8.246	7.021
	λ (day)	8.354	5.72	9.159	5.715	6.299	5.328
Modified Gompertz	R^2	0.9960	0.9941	0.998	0.9956	0.9973	0.9945
	RMSE	5.141	5.150	4.603	6.201	4.245	5.47
	$P(Nl. (kg VS)^{-1})$	319.9	266.1	482.5	450.5	337.8	352.4
	$r_m(Nl. (kg VS. day)^{-1})$	7.62	6.185	9.628	8.318	7.584	6.52
	λ (day)	6.696	4.085	7.458	4.012	4.59	3.637

P: maximum specific biogas production potential, r_m : max. Specific biogas production rate, λ : lag-phase, t: incubation time, RMSE: Root Mean Square Error, R^2 : correlation coefficient

Figure 4 shows a relative decrease in the pH of the fermenting medium in the first week of anaerobic digestion in runs A, B and C however, the pH values fluctuated in the acceptable range except for run B that pH dropped to 6.7 after 30th day. The pH of the digester content remained steady state and showed lower fluctuations with regards to variation in OLR indicating that the digestion in reactor was well buffered and maintained in the suitable range for the methanogenesis. Enhancements of biogas yield due to increment of pH probably the result of addition metabolic activity of the microbial community that is exist in the digester (Lyberator & Skiades, 1999). It has been reported that anaerobic bacteria required a natural environment and thus a pH ranging from 6.4 to 7.2 is needed for optimum biogas production (Rabah *et al* 2010).

3.3. Kinetic model of biogas production

Kinetic parameters of fermentation process are always useful in comprehension inhibitory mechanisms of bio decomposition and are applied to analyses the efficiency of reactors and design the appropriate reactors (Li *et al.*, 2014). Fig. 5(a), 5(b), 5(c), 5(d), 5(e) and 5(f) demonstrate the biogas accumulation simulation, using Modified Gompertz and Logistic kinetic plots along with observed values of specific cumulative biogas production data from single digestion of CM and co-digested CM+CSR for OLRs of 2 and 3 kg VS.(m⁻³.d⁻¹), respectively. The Modified Gompertz and Logistic kinetic plot had the highest correlation and lower RMSE for simulating biogas accumulation.

The coefficient of determination (R^2) obtained as 0.9960, 0.9941, 0.998, 0.9956, 0.9973 and 0.9945 using modified Gompertz kinetic model and (0.990, 0.9995,

0.9954, 0.9924, 0.9942 and 0.9905) by applying Logistic kinetic model for runs A, B, C, D, E, and F, as shown in Table 4, respectively. Therefore, both the modified Gompertz and logistic kinetic model could be used to simulate methane production by a completely stirred tank reactor (CSTR) under semi-continuous feeding circumstance.

In the Logistic kinetic equation, the kinetic rate constant was found to be in the order of biogas production (263.1, 223.2, 360.4, 345.8, 275.9 and 373.4)

LN. kg VS⁻¹ input at 42th day for runs A, B, C, D, E and F respectively. The maximal biogas production rate r_m and lag phase period (λ) was found to be presented in table 4. Thus, in modified Gompertz equation, the potential of biogas production (P) was found to be in the order of specific normal biogas production at (319.9, 266.1, 482.5, 450.5, 337.8 and 352.4) LN. kg VS⁻¹ input at day 42 for runs A, B, C, D, E and F respectively. Biogas production rate (r_m) and lag phase period (λ) was found to be presented in Table 4.

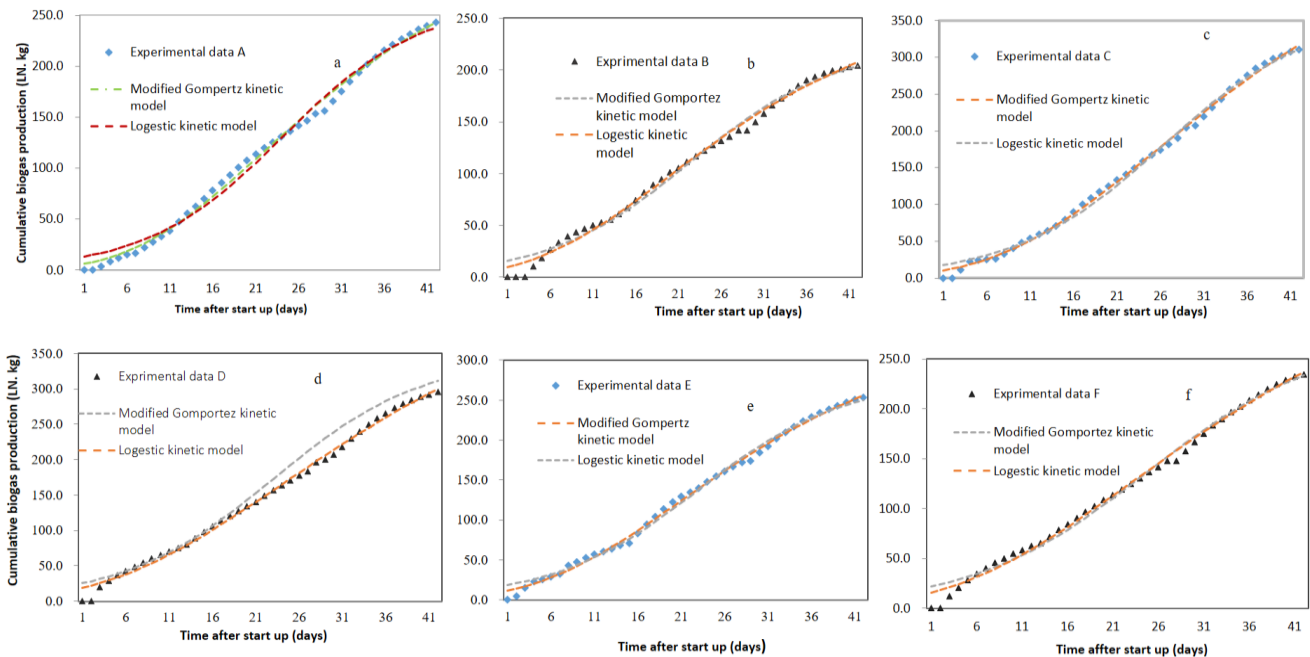


Figure 5. Kinetic growth models of modified Gompertz and logistic equations fitted to the specific cumulative methane production data in different runs (a) only CM with OLR=2, (b) only CM with OLR=3, (c) 75% CM + 25% CSR with OLR=2, (d) 75% CM + 25% CSR with OLR=3, (e) 50% CM + 50% CSR with OLR=2 and (f) 50% CM + 50% CSR with OLR=3

4. Conclusion

The anaerobic CSTR which was employed under semi-continuous feeding circumstance during this study demonstrated an acceptable performance along both single digestion of cow manure and Co-digestion of cow manure with corn straw residue although co-digestion experimental runs showed better results in terms of pH stability and specific methane production. The methane content (54-63%) and VS reduction of around 55-74% in different runs represented promising process efficiency under the practical conditions of anaerobic digestion operations. In addition, Modified Gompertz and Logistic kinetic modeling plots had higher correlation than exponential rise to maximum plot for simulating biogas production.

Therefore, with increasing the environmental concerns and predominant wastes management crises, optimizing biogas production is effective way to reduce GHG emissions in terms of the of generation renewable energy by co-digestion of agricultural and animal waste.

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