Effect of Sulfur Addition to Nickel Recovery of Laterite Ore

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1. Introduction

Laterite ore is the primary source of nickel, which covers 60% of the total nickel reserves in the world [1]. Laterite ore is widely distributed, especially in the tropics. Based on data from the ESDM Data Review Center in 2012, in Indonesia alone, the potential for laterite nickel was estimated at 1.878 million tons with an average nickel content of 1.45% spread across Sulawesi, Kalimantan, Maluku, and the Papua regions [2]. The amount of reserves is ranked fourth in the world, with a percentage of 12% [3]. This potential certainly provides an excellent opportunity for Indonesia because of the increased projected demand for nickel until 2025, while world nickel production tends to decrease due to the depletion of nickel sulfide reserves [4, 5].

Laterite nickel is usually formed as a residual product of chemical weathering in ultramafic rocks that contain ferromagnetic materials such as olivine, pyroxene, and amphibole. Laterite ores have an average of <2% nickel content, which is generally in the goethite (FeOOH) crystal lattice [6]. Nickel is spread out throughout the ore, and it is difficult to increase its content using the usual physical beneficiation method [3]. This condition prompted the researchers to develop new methods, one of which is through the reduction roasting pathway, which reduces NiO to metallic nickel and separates it from iron impurities [7]. This process is possible to be carried out thermodynamically, but in practice, there are problems in determining the reduction temperature. At 600°C, NiO has been reduced to metallic nickel, but the particle size is still too small to be separated by magnetic separation [8]. Conversely, if the reduction process is carried out at a
temperature of 1000°C will produce large metallic particles, but the reduction rate of Fe oxides also increases, which causes a decrease in nickel content[9].

Several previous studies have shown that the reduction of metallic particles can be enlarged by adding additives containing sulfur. Some additional elements, such as adding iron content to the ore, can also increase nickel yield [10]. But at this time, the addition of sulfur is widely studied because sulfur is known to reduce the surface tension of metal particles so that the particle size can grow larger [11]. Zhu et al. [12] roasted laterite nickel reduction at 1100°C for 60 minutes with a 6% CaSO₄ additive. From his research, the ferronickel concentrate was obtained with 6% Ni content and 92.1% recovery. Setiawan et al. [13] conducted a study of carbothermic reduction using sub-bituminous coal containing sulfur, which was followed by magnetic separation, and the result obtained was an increase in nickel content up to 5% (weight). Li et al. [14] conducted a study of nickel laterite reduction at 1100°C for 60 minutes with the addition of 20% Na₂SO₄ additive. The result is a ferronickel concentrate with Ni content reaching 9.48%, but the recovery is only 83.01%.

This research was conducted to determine the right combination between the amount of reducing agent and sulfur to be added in the process of selective reduction of laterite nickel reduction with graphite reducing agent and the addition of sulfur additives. The effect of process variables such as reduction time, reductant addition, temperature, and sulfur addition was determined quantitatively.

2. Methodology

2.1. Material and Tools

The raw material used in this study was laterite ore from Sangaji Halmahera. The chemical composition of laterite ore samples was analyzed using XRF (X-Ray Fluorescence) Panalytical Epsilon 1. The results showed that the iron and silica content in laterite ore was quite high, 69.6%, and 14.8%, respectively, as Fe₂O₃ and SiO₂. The total Ni contained in the ore was quite low, only around 1.11%. XRD analysis (X-Ray Diffraction), which is a qualitative analysis of minerals, was then determined using PANalytical X’Pert Pro MPD XRD with Cu Ka radiation (λ = 1.5406 Å). The generator was operated at a voltage of 40 kV, an electric current of 30 mA, a measurement speed of 2°/min, and a sampling pitch of 0.020°. Following the results of previous studies, it was known that the laterite ore used was a type of limonite which was dominated by the structure of the mineral goethite and had low Ni contents [15]. The compounds contained in the ore consist of quartz minerals (SiO₂), goethite (FeO(OH)), hematite (Fe₂O₃), and lizardite (Mg₃(Si₄O₁₀)(OH)₆) [16]. Limonite ore was first dried in an oven for 12 hours at a temperature of 110°C, crushed with a jaw crusher, crushed with a disk mill, then sieved to obtain granules with a size of 74 microns.

In the reduction process, graphite reductant was used as carbon sources, with a fixed carbon value of 96.8% to minimize the effects of impurities such as volatile matter and water content on the reduction process. Additives added in the form of sulfur from nature. The graphite and sulfur that was used go through the process of crushing, grinding, smoothing and sieving like the limonite ore to pass a 44-micron sieve to ensure that the material was entirely distributed in the mixture of material to be reduced. Laterite ore was then mixed with graphite and sulfur in a specific ratio then formed into pellets to obtain an even heat distribution during the reduction process.

2.2. Experiment

Selective reduction experiments were carried out in a Carbolite CWF 1300 type muffle furnace. A certain amount of pellet was inserted into a graphite crucible and covered with a layer of glass wool and charcoal to ensure the conditions inside the crucible remained reductive. The crucible containing the sample was put into a muffle furnace at room temperature. The furnace was heated to a certain temperature then held with a variation of the reduction time of 30-180 minutes. The reduction temperature was 800-1100°C, as well as the addition of reductant agents and additives, each of which was 0-21%. The reduced sample was cooled slowly in the furnace until it reached room temperature, then permanently separated (permanent hand magnetic) therefore, there was a separation between the concentrate containing a lot of ferronickel metal and tailings. The concentrate was weighed and analyzed using XRD (X-Ray Diffraction) and AAS (Atomic Absorption Spectrophotometer).

The addition of reductants and additives was based on the stoichiometry calculation of the reactions that occurred, then the amount was varied with less amount than stoichiometry and exceeded stoichiometry.

Analysis of Ni and Fe content was calculated based on measurement results using AAS (Atomic Absorption Spectrophotometer), while the recovery was calculated using equation (1):

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\% \text{Recovery} = \frac{\text{metal content in concentrate \times mass of concentrate}}{\text{metal ore content \times ore mass}} \times 100\% \quad (1)
\]

3. Result and Discussion

The effect of various parameters of the reduction process was carried out by determining changes in the contents of Ni and Fe in the reduction process product concentrate, as well as the percentage of its recovery.

3.1. Effect of Reduction Time

One of the variables that significantly influence the results of the selective reduction process was the length of the reduction process. Theoretically, the longer the reduction process, the more metal phase formed [17]. The reduction time was varied for 30, 60, 120, and 180 minutes with a temperature of 1100°C, the reducing agent and sulfur were 7% by weight of the limonite ore sample,
respectively. The results of the AAS analysis of the reduced Ni and Fe contents at various time variations are shown in Figure 1.

![Figure 1. The effect of reduction time to the concentrate of reduction product (a) the content of Ni and Fe (b) the recovery of Ni and Fe](image)

Figure 1 shows that in the first 30 minutes of reduction, Ni contents increased from 1.11% in the initial sample to 1.24%. The maximum increase in Ni contents reached 1.34% after a reduction of 180 minutes. Increasing Ni contents caused a decrease in Fe contents so that the tendency of the curve is vice versa. Overall, the Fe content decreased significantly from the initial sample that had a total Fe content of 48.72% to 24.2% with a reduction time of 60 minutes. The decrease in Fe contents was also accompanied by a significant decrease in Fe recovery from a reduction time of 30 minutes to 60 minutes. The addition of a reduction time of 180 minutes increases the reduction in Ni recovery by 25% with a less significant decrease in Fe recovery. Therefore, 60 minutes is the optimum reduction time because there is an increase in Ni contents that were obtained with a substantial reduction in Fe recovery. That is possible due to the influence and the presence of sulfur, which were added as additives in the reduction process. Sulfur can bind iron to become FeS and increase the nickel content of the reduced product concentrate [18]. A description of the reactions that occur between Fe and S is presented in more detail in section 3.4. The longer the reduction time, the higher the Fe metallization, hence the higher the FeS formed and separated in the tailings. This causes the number of residues to increase, and the recovery of concentrates gets smaller, so, despite an increase in Ni contents, the percentage of recovery is small.

3.2. Effect of Reduction Temperature

The effect of the reduction temperature on the reduction process was observed at temperatures of 800, 900, 1000, and 1100°C. The selection of the reduction temperature variable was based on the Gibbs energy of metal oxides NiO, FeO, and FeO, and data on the decomposition process of TG-DTA testing on a mixture of limonite and graphite ores that have been performed in previous studies [16, 19]. NiO, FeO, and FeO metal oxides can be reduced using carbon to Ni, FeO, and FeO at the lowest temperatures of 435, 798, and 1187°C, respectively [20].

The reduction experiment for each temperature was carried out for 60 minutes with the addition of graphite reductant and sulfur additives, each of 7% of the sample weight. Then the reduction of product concentrate was analyzed using AAS to determine the contents of Ni and Fe metals. Changes in Ni and Fe metals are shown in Figure 2.

![Figure 2. The effect of reduction temperature to the concentrate of reduction product (a) the content of Ni and Fe (b) the recovery of Ni and Fe](image)

After the reduction process, there was an increase in Ni metal content and recovery percentage. Meanwhile, for Fe metals, the content continues to increase as the temperature of the reduction increases, while the percentage of recovery decreases. In Ni metal, the Ni content in the reduction product concentration increased from 1.49% to 1.98% with a maximum gain of up to 96%
at an increase in temperature from 800 to 1100°C. The Fe metal content increased from 24.7% to 29.2%, with the recovery percentage decreased from 76.1% to 70% due to the same temperature rise. This decrease in the recovery is due to the reduction of oxides that react with carbon so that the mass of the initial sample decrease with increasing temperature. The maximum value is reached at 1100°C due to the formation of the kamacite phase. This phase initiates the formation of FeS, which can be separated in the tailings; therefore, Ni contents and recovery increase.

Temperature is a factor that significantly influences the reduction process [21]. The increasing temperature is causing reduction to take place more correctly, as evidenced by increasing metal content [11]. From the kinetics point of view, an increase in temperature should result in metallic iron and nickel becoming agglomerated and growing into larger particles [12], as well as increasing the liberation of Ni and Fe-silicates [9]. However, a decrease in the percentage of Fe recovery shows that in the temperature range, the reaction to the formation of Pyrhotite (FeS) is easier than the reduction of iron and nickel. This is in accordance with the study of Zhu et al. [12] that the reduction process with the addition of CaSO₄ increased the formation of fayalite (Fe-silicate), which inhibited wustite reduction. More about the effect of adding sulfur to the reduction process is explained in the next sub discussion.

To illustrate the effect of temperature on the reduction of limonite nickel ore, the concentrate of reduction product sample was analyzed using XRD to see the mineral structure formed after the reduction process. The results are shown in Figure 3.

![Figure 3](image_url)

**Figure 3.** XRD diffractogram of concentrate product reduction at various temperatures.

Based on Gibbs free energy data (ΔG°) for metal oxides, NiO has been reduced starting at temperatures of ~430-440°C while Fe₂O₃ and FeO₆ can be reduced using carbon to FeO₃ and FeO at temperatures of 798 and 1187°C, respectively [20]. At a reduction temperature of 800 and 900°C, magnetite Fe₃O₄ was formed as a result of the reduction of hematite (Fe₂O₃). Starting at a temperature of 1000-1100°C, the phases of Kamasite (Fe-Ni), Pyrhotite (FeS), Olivine (Mg-Fe-Silicate), and Magnesiophyrite (FeMgO₆) were presented. Temperature reduction at 800°-900°C has not given good results for increasing contents and recovery of Ni because the decomposition of graphite as a reducing agent is low. Figure 3 shows that at a temperature of 1000°C, the carbon intensity decreases significantly, accompanied by the presence of the kamacite and FeS phases, thereby increasing the reduction temperature to 1100°C. Carbon can be decomposed as a whole, and the intensity of kamacite increases, so the higher the rate of formation FeS phase can be seen from the higher intensity of the FeS phase peak.

### 3.3. Effect of Addition of Reducing Agent

The more amount of reducing agent added, the higher the content of the metal element in the reduction product concentrate. In this study, the amount of graphite added to the limonite ore sample was 0, 5, 10, and 21% by weight of the sample. The reduction took place at a temperature of 1100°C for 180 minutes, with the addition of an additive of 7% by weight followed by magnetic separation. The results of the analysis of changes in the contents of Ni and Fe in the reduction product concentrate and the percentage of recovery of Ni and Fe can be seen in Figure 4.

![Figure 4](image_url)

**Figure 4.** The effect of the amount of reducing agent to the concentrate of reduction product (a) the content of Ni and Fe (b) the recovery of Ni and Fe.
Both iron and nickel have the same tendency towards the effect of reducing agent addition. The addition of 14% reductant led to an increase in contents and recovery, which respectively reached 29.1% and 68.2% for iron, and 1.74% and 89.4% for nickel. Furthermore, the value decreases due to the addition of reducing agents by 21%.

The addition of the number of reducing agents allowed the formation of increasingly reductive conditions for the reduction reaction to take place because the CO gas formed upsurged, so it pushed the reaction towards the formation of nickel and iron metals. This was indicated by the increasing contents of Ni and Fe metals in the concentrate of reduction product along with the rise in the amount of graphite added. However, if the reductant was added excessively the process of agglomeration of small metal particles into larger metal particles was more difficult because besides being hindered by the presence of carbon atoms, the condition of the ore will be less “viscous” so that the movement of metal particles during the reduction process will be hampered [22]. Li et al. [14] stated that when the carbon content has reached an optimal value, the subsequent addition of carbon cause the formation of large amounts of carbon residues, which hinder the process of reduction.

### 3.4. Effect of the Addition of Sulfur

The reduction experiment was carried out by adding a 14% reductant amount and varying the amount of sulfur added by 0, 7, 14, and 21% by weight of the limonite sample. The reduction reaction was carried out at 1100°C for 60 minutes. After the reduction is carried out, continued with magnetic separation to produce a concentrate. Changes in the contents of Ni and Fe in the reduction product concentrate, as well as the percentage of recovery of iron and nickel obtained can be seen in Figure 5.

Until the addition of sulfur of 7%, Ni contents increased and reached 1.61% and then decreased with the next addition of sulfur. The maximum percentage of recovery for Ni was 79.2%. With respect to Fe content and percent recovery, the addition of sulfur to the reduced ore tends to cause a decrease of the maximum value of 34.5% and 87.7%, respectively. This decrease in iron recovery indicates that sulfur influences the selective reduction of laterite nickel ore by the formation of FeS compounds [18]. However, the increase in the percentage content and recovery of Fe occurs with the addition of 14% sulfur, and this can be due to the presence of Mg, Fe-SiO₂ phase as shown in Figure 6, where the phase is paramagnetic so that it is possible to increase the amount of magnetic separation increasing the percentage of Fe content and recovery[23].

**Figure 5.** The effect of the amount of sulfur on the concentrate of reduction product (a) the content of Ni and Fe (b) the recovery of Ni and Fe

The combination of controlling the reducing agent contents with the addition of appropriate sulfur compounds makes metallic nickel growth increase [5]. In general, ore, which is roasted with the addition of sulfur, has a loose structure, and FeS cover the metal particles. Sulfur will cover the surface of metallic iron particles and react to form FeS by reaction (1) [18].

\[
Fe + S \rightarrow FeS
\] (1)

The formation of FeS in the reduction process by the addition of sulfur can be explained through the XRD graph, as shown in Figure 6. It can be seen that the reduction process without the addition of sulfur causes the formation of the Kamasite (FeNi) phase with a high enough intensity and the Magnesiopherite (FeMgO₃) phase is also detected. As the amount of sulfur added to the ore decreases, it increases. The kamacite phase decreases in intensity, followed by the formation of the pyrrhotite (FeS) phase, whose intensity is increasing. As the pyrrhotite (FeS) phase increases, the relative content of nickel to iron in the concentrate will increase.
4. Conclusion

The limonite type of nickel laterite ore reduction process is influenced by the reduction time and temperature, as well as the number of reducing agents and additives. The reduction temperature at 1100°C can cause the reducing agent to decompose as a whole so that the intensity of kamacite increases. The addition of sulfur additives to a certain amount can increase the content and percentage of nickel recovery from limonite type nickel laterite ore by suppressing the metallization of iron due to FeS formation. The formation of Fe-silicate, which is paramagnetic and has the potential to increase contents and the recovery of Fe can be overcome by adding sulfur additives of 7% and a reduction temperature at 1100°C. The reduction process can be carried out for 60 minutes because although Fe recovery can be reduced by increasing the reduction time, nickel recovery will also decrease significantly if the reduction time is increased.

References


