



# Effect of Carbonization Step on Surface Character of Activated Carbon from Cassava Peels and Its Simple Application for BTEX Adsorption

Cucun Alep Riyanto <sup>1,\*</sup>, Alvama Pattiserlihun <sup>2</sup>, Blessy Yemima Andiani <sup>1</sup>, Ezra Kurniawan <sup>1</sup>, Fahmi Puteri Perdani <sup>1</sup>, Marcelino Kelpitna <sup>3</sup>

<sup>1</sup> Department of Chemistry, Faculty of Science and Mathematics, Satya Wacana Christian University (UKSW), Salatiga, Indonesia

<sup>2</sup> Department of Physical Education, Faculty of Science and Mathematics, Satya Wacana Christian University (UKSW), Salatiga, Indonesia

<sup>3</sup> BMT Laboratory, Bogor, Indonesia

\* Corresponding author: [cucun.riyanto@uksw.edu](mailto:cucun.riyanto@uksw.edu)

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## Abstract

Activated carbon is obtained from biomass waste because it is cheaper and renewable from an environmental perspective. In cassava peel biomass waste, it is necessary to study the effect of the carbonization stage on the surface character and pore distribution of the activated carbon obtained. In this research, the study of the impact of the carbonization stage is continued with the application of adsorption to volatile compounds, specifically benzene, toluene, ethylbenzene, and xylene (BTEX). This study conducted carbonization at 400°C (t: 60 minutes) followed by dual activation stages, namely chemical activation (carbon: H<sub>3</sub>PO<sub>4</sub> 30%, ratio 1:5, w/b) and physical activation (furnace, T: 600°C, t: 60 minutes). After that, the activated carbon from cassava peels (CPAC) was applied as an adsorbent for BTEX. The results showed that CPAC has an amorphous character with O-H, C-H, C≡C, C=C stretching, C-O, and C=N functional groups. The carbonization step changes pore properties. CPAC-202 (with carbonization) has a mesoporous character with a surface area up to 198.233 m<sup>2</sup>/g, with the surface dominated by C and O elements. The selectivity of BTEX gas adsorption is more significant for toluene using CPAC-202, with the best adsorption reaching 6.418 mg/L.

## 1. Introduction

Activated carbon is well known as an adsorbent despite various other applications, mainly due to their nature of being highly porous nature with a large surface area to facilitate adsorption [1]. Activated carbon can be produced from a variety of raw materials, such as biomass waste from agricultural products [2]. Agricultural biomass waste used as a material for making activated carbon has the advantage of being cheaper, easier to use, and renewable in environmental aspects [3]. This is based on its high economic value and the presence of chemical compounds in agricultural waste. One of the agricultural wastes that has received special attention is cassava peel.

In some processing countries, cassava peels pose a disposal challenge as waste from staple foods [4]. Cassava

peel (*Manihot esculenta* Crantz) accounts for 10–20% of the total weight of cassava, making it a potential candidate for utilization in biotechnology and on an industrial scale [5]. The hemicellulose content of 23.9% and the lignin content of 7.5% [6] indicate that cassava peels exhibit a significant ability as a metal-binding material from aqueous solutions [7]. Based on FAO data in 2018, Indonesia became the third-largest cassava-producing country in the world, with production reaching 25 million tons by the end of 2015 [6], indicating significant potential for developing activated carbon sources from cassava peels. The activated carbon derived from biomass, such as cassava peels, is highly regarded for its renewability, environmental friendliness, and broad potential for applications [8].

One of the stages in the manufacture of activated carbon is the activation process, because this stage is used to enlarge the sorption area and pore volume in activated carbon [9]. Activator substances such as  $\text{ZnCl}_2$  and  $\text{H}_3\text{PO}_4$  are commonly used for materials containing lignocellulose [10]. According to Jaria *et al.* [11],  $\text{H}_3\text{PO}_4$  has several advantages over other chemical activators, such as being friendly to the environment, requiring low energy in the activation process, and being economical (eco-friendly).  $\text{H}_3\text{PO}_4$  activator also produces higher yields of activated carbon and has non-toxic properties, making it safe for use in the food and pharmaceutical industries [12]. Nicha *et al.* [13] synthesized the activated carbon derived from palm shells treated with 10%  $\text{H}_3\text{PO}_4$ , the material produced larger and cleaner pores due to the effective removal of surface residues.

Another stage in the activated carbon fabrication process is carbonization. Carbonization is a physical activation process used to remove water and volatile matter from biomass, and pore formation by the formation of  $\text{CO}_2$  and heat [2, 14]. During the carbonization process, volatile matter decreases, and fixed carbon increases [15]. Research El-Hendawy *et al.* [16] conducted carbonization at  $500^\circ\text{C}$  and continued chemical activation and pyrolysis at  $700^\circ\text{C}$  to produce activated carbon with a high surface area that has good adsorption capacity for methylene blue and  $\text{Pb}^{2+}$ . Further analysis is needed to know about the impact of the carbonization process on pore formation and the surface characteristics of the material.

Activated carbon, with its large surface area, has the potential to be used as an adsorbent for volatile organic compounds (VOCs). The adsorption method is considered more economical and environmentally friendly than other methods, such as catalytic degradation, biodegradation, and membrane technology [17]. Research by Wu *et al.* [18] on toluene adsorption using Fe-modified activated carbon fiber resulted in a toluene adsorption capacity of 218.12 mg/g. Apart from toluene, VOC adsorption can also be carried out on BTEX (benzene, toluene, ethylbenzene, and xylene) using activated carbon from eucalyptus leaves, which has a surface area of  $128 \text{ m}^2/\text{g}$  and is effective as a BTEX adsorbent, achieving a removal efficiency of 94% [19]. BTEX is commonly found in the environment, primarily due to industrial activities and the use of fossil fuels. These compounds are highly volatile, meaning they can easily vaporize into gas at room temperature, making them a significant air pollutant, especially in areas close to industrial activity, such as the petroleum industry and factories with chimneys [20].

Based on several studies conducted, this research specifically examines the effect of the carbonization stage on the surface characteristics and pore distribution of activated carbon derived from cassava peels (CPAC) biomass waste. The CPAC obtained is then used as a BTEX adsorbent to determine the significance of the carbonization stage.

## 2. Experimental

### 2.1. Tools and Instruments

The tools used in this study were a balance analytical with an accuracy of 0.01 g (Ohaus TAJ601), an analytical balance with an accuracy of 0.1 mg (Ohaus PA214), a pH meter (Hanna HI 9812), a furnace (Vulcan A-550), an oven, a grinder, a 30 and 60 mesh sieve, a porcelain cup, a reflux device, and a vacuum Buchner.

The instruments used to characterize the activated carbon results were a Fourier Transform Infrared spectrophotometer (FTIR, Shimadzu Prestige 21, Gadjah Mada University), an X-ray Diffractometer (XRD, PANalytical X'Pert Pro, State University of Malang), a Scanning Electron Microscope (SEM, Phenom Dekstop ProXL, Islamic University of Indonesia), a Surface Area Analyzer (SAA, Quantachrome NOVA 1200e, Semarang State University), and Gas Chromatography with Flame Ionization Detection (GC-FID, Agilent Technologies GC Model 7890A, PT. ALS Indonesia - Bogor).

### 2.2. Materials

Cassava peels were obtained from the Ledok Cassava Industry Center in Salatiga. The chemicals used included distilled water from the Chemistry Laboratory of Satya Wacana Christian University (UKSW), commercial activated carbon purchased from chemical suppliers, and  $\text{H}_3\text{PO}_4$ ,  $\text{NaOH}$ , and  $\text{HCl}$ , all of which were PA-grade (Pro-Analysis) reagents from E-Merck, Germany. The BTEX stock standard solution (1000 mg/L) from the Absolut Standard was obtained from ALS Laboratory, Bogor.

### 2.3. Raw Material Preparation

The cassava peels were cleaned of soil or impurities, and then the white part was separated from the outer skin. The white part was washed with clean water, cut into small pieces ( $4 \times 4 \text{ cm}$ ), and then dried in the sun for 2 days. After 2 days of drying, the samples were oven-dried at  $110^\circ\text{C}$  for 24 hours. The dried samples were then pulverized with a grinder and sieved using a 30-mesh sieve [21].

### 2.4. Carbonization and Activation Process

In the stage without carbonization, the sieved samples were impregnated with 30%  $\text{H}_3\text{PO}_4$ , using a carbon: phosphoric acid impregnation ratio of 1:5 (w/w) for 24 hours. The impregnation results were then filtered and oven-dried at  $110^\circ\text{C}$  for 24 hours. Afterward, they were activated in a furnace for 1 hour at an activation temperature of  $600^\circ\text{C}$ . The activated carbon was neutralized with a 1 M  $\text{NaOH}$  solution and rinsed with distilled water until the pH reached 7. The activated carbon was then oven-dried at  $110^\circ\text{C}$  for 24 hours and then stored and labeled CPAC-201 (without carbonization) [22].

At the carbonization stage, the sieved samples were carbonized in a furnace at  $400^\circ\text{C}$  for 1 hour. The carbonization results were cooled to room temperature, and then the carbon was activated using a 30%  $\text{H}_3\text{PO}_4$  solution with a carbon-to-phosphoric acid impregnation ratio of 1:5 (w/w) for 24 hours. The impregnated carbon

was then filtered, oven-dried at 110°C for 24 hours, and put back in the furnace at 600°C for 1 hour. The activated carbon was neutralized with a 1 M NaOH solution and rinsed with distilled water until the pH reached 7. The activated carbon was then oven-dried at 110°C for 24 hours and stored and labeled CPAC-202 (with carbonization) [21, 23, 24].

## 2.5. Material Characterization

The analysis of functional groups in CPAC was conducted using FTIR within the wavenumber range of 4000–400  $\text{cm}^{-1}$ . The crystal properties of CPAC were examined using XRD. Surface morphology was analyzed using an SEM to observe surface structures, while pore size and distribution were evaluated using an SAA.

## 2.6. Adsorption of BTEX

The BTEX adsorption process was conducted according to NIOSH Method 1501 for hydrocarbons and aromatic compounds. A personal air sampling pump (Gilibrator DBX II), calibrated to operate at a flow rate of 0.01–2 L/min, was used in the setup. The adsorbents employed were CPAC-201 and CPAC-202. A total of 1 g of each adsorbent was placed into a BTEX adsorption simulator and connected via tubing to the personal pump set to a specific flow rate. The adsorption process was conducted during the evaporation of 1 mL of a standard BTEX solution (purged with  $\text{N}_2$ ), prepared in varying concentrations. After the adsorption process, the BTEX compounds were desorbed from the adsorbent using CS/DCM, and the concentrations were then analyzed using GC-FID.

Gas chromatography analysis was performed using an Agilent Technologies GC Model 7890A equipped with a Flame Ionization Detector (FID). The injector (A) was set at 225°C, and the detector (FID-A) at 250°C. The column used was HP-1 MS (30 m  $\times$  320  $\mu\text{m}$   $\times$  0.25  $\mu\text{m}$ ). Nitrogen was used as the carrier gas at a flow rate of 2.5 mL/min. The oven temperature program began at 40°C (held for 1 minute), followed by Ramp 1 at 10°C/min for 8 minutes, and Ramp 2, which reached a final temperature of 120°C and was held for 2 minutes, resulting in a total run time of 11 minutes. The nitrogen purge for the septum was maintained at 3 mL/min. The injection volume was 1  $\mu\text{L}$ .

## 3. Results and Discussion

### 3.1. FTIR Characterization of CPAC

The FTIR results shown in Figures 1b and 1c display absorption peaks at wavenumbers 3425.58, 2931.80, 2337.72, 1620.21, and 1157.29  $\text{cm}^{-1}$ , corresponding to the vibrations of O–H, C–H,  $\text{C}\equiv\text{C}$ , C=C stretching, and C–O stretching, respectively [25]. These peaks are similar to those observed in commercial activated carbon (CAC). Additionally, Figures 1b and 1c exhibit a broader peak at 1566.20  $\text{cm}^{-1}$  compared to Figure 1a, indicating the presence of C=N stretching vibrations, which are associated with cyanide compounds found in cassava peel [26]. The identified functional groups and their respective absorption regions in the activated carbon samples are summarized in Table 1.

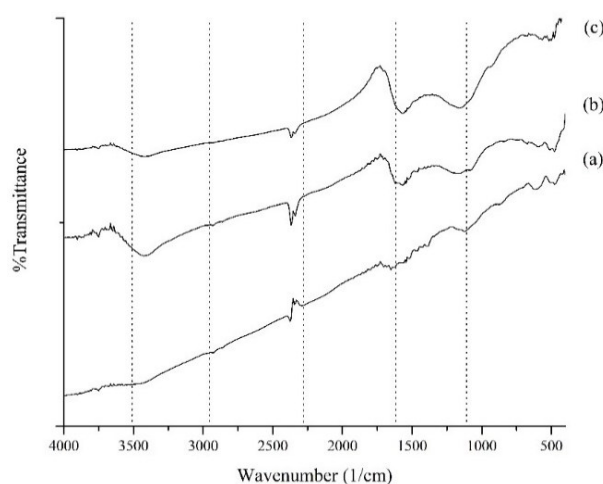


Figure 1. FTIR spectra of a) CAC, b) CPAC-201, and c) CPAC-202

Table 1. Functional groups of activated carbon

Wavenumber of activated carbon ( $\text{cm}^{-1}$ )					
No.	Functional group	Theoretical [27]	CAC	CPAC-201	CPAC-202
1	O–H	3570 – 3450	3510.45	3425.58	3425.58
2	C–H	2975 – 2915	2931.80	2931.80	2931.80
3	$\text{C}\equiv\text{C}$	2260 – 2190	2291.43	2337.72	2337.72
4	C=C	1660 – 1580	1635.64	1620.21	1620.21
5	C=N	1570 – 1515	–	1566.20	1566.20
6	C–O	1200 – 1050	1126.43	1157.29	1157.29

### 3.2. XRD Characterization of CPAC

The diffractogram of standard activated carbon (Figure 2a) shows the appearance of a wide angular range and the absence of sharp peaks in the activated carbon diffractogram, indicating the dominant structure is amorphous [25]. The diffractogram pattern of standard activated carbon shows two peaks at diffraction angles of  $\sim 24^\circ$  and  $\sim 44^\circ$  (weak) (Figure 2a).

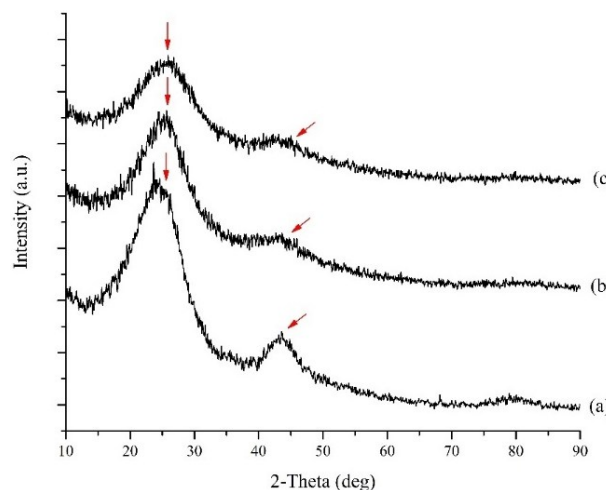


Figure 2. X-ray diffractogram of a) CAC, b) CPAC-201, and c) CPAC-202

The XRD patterns of CPAC-201 (Figure 2b) and CPAC-202 (Figure 2c) show two diffraction peaks at angles of  $\sim 25^\circ$  (medium) and  $\sim 43^\circ$  (weak). These results show a diffraction pattern similar to that of standard activated carbon (Figure 2a). Therefore, the preparation of CPAC without or with carbonization has no significant impact on the crystalline or amorphous character of the CPAC produced.

### 3.3. Surface and Pore Analysis of CPAC

In the surface analysis of CPAC-201 and CPAC-202, the results in Figures 3 and 4 show that the surface image in the process without carbonization (CPAC-201) is homogeneous and non-porous, while with carbonization (CPAC-202), it tends to be homogeneous, and pores are formed. In the elemental composition analysis, both CPAC surfaces are dominated by the element carbon (C), with a percentage exceeding 50% in both atomic and mass percentages. The presence of phosphorus (P) and sodium (Na) elements is expected due to the use of  $\text{H}_3\text{PO}_4$  and NaOH in the process of making cassava peel-activated carbon. In Figure 4, a percentage of the element nitrogen (N) is presented, which supports the previous characterization data obtained using an FTIR spectrophotometer, showing the stretching vibrations of the C=N bond of the cyanide compound present in cassava peel.

The carbonization significantly impacts the pore properties of activated carbon materials, primarily influencing pore development, size, volume, and surface area. Carbonization promotes the release of volatile compounds, creating initial pores in the carbon structure. Efficient thermal decomposition of volatile matter increases surface area and micropore volume due to more complete carbonization [26]. Elevated carbonization temperatures tend to favor micropore and mesopore development, as more volatile components are removed, leading to increased pore volume and specific surface area [28].

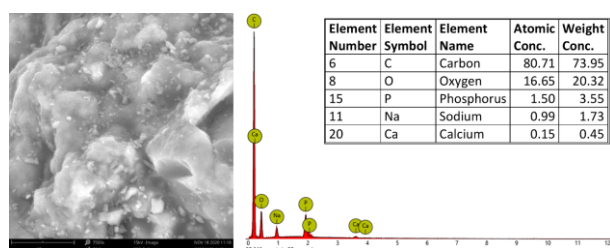


Figure 3. SEM image and element composition on the CPAC-201 surface

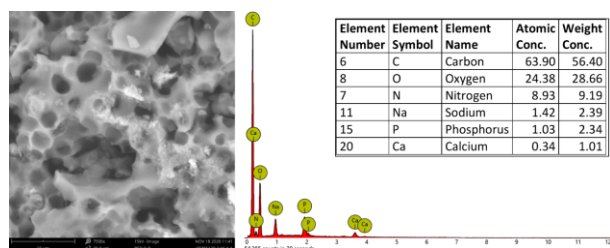


Figure 4. SEM image and element composition on the CPAC-202 surface

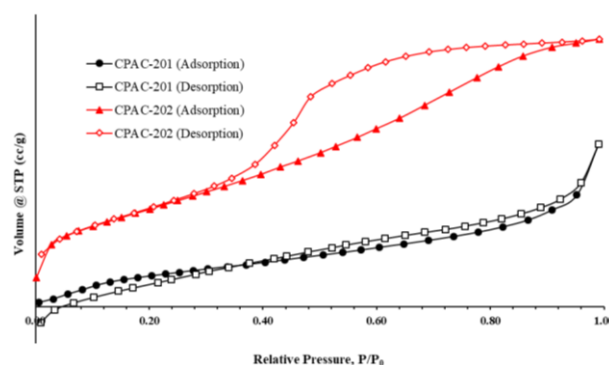


Figure 5. Nitrogen adsorption-desorption isotherm of CPAC samples

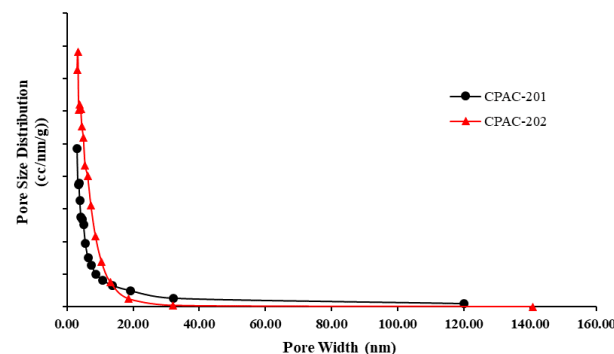


Figure 6. Pore size distribution of CPAC samples

CPAC samples, produced with and without carbonization, were analyzed using the BET method to determine surface area, pore characteristics (microporous or mesoporous), and total pore volume. The complete BET analysis results are presented in Figures 5 and 6, as well as in Table 2. The analysis was conducted based on nitrogen adsorption-desorption isotherms using relative pressure ( $P/P_0$ ).

Based on Figure 5, CPAC-201 follows a type II isotherm plot, indicating predominantly non-porous or macroporous characteristics, whereas CPAC-202 follows a type IV isotherm associated with capillary condensation in mesopores and a limiting uptake at high  $P/P_0$ . CPAC-202 also exhibits a strong H2-type hysteresis loop, reflecting the differences between adsorption and desorption mechanisms in ink-bottle-type pores with narrow necks and wider bodies [29]. The H2 loop is associated with non-uniform, often irregular or elongated pores, with significant connectivity between pores, possibly forming a network that impacts fluid condensation and evaporation dynamics [30].

The pore characteristics of CPAC-201 and CPAC-202 show pore diameters in the nanoscale range ( $< 10$  nm) (Figure 6). The average pore sizes are 3.84 nm for CPAC-201 and 2.28 nm for CPAC-202, placing both within the mesoporous category (2–50 nm) [31]. Additional parameters, including surface area and pore volume, are summarized in Table 2. However, CPAC-201 exhibits a very low surface area ( $4.773 \text{ m}^2/\text{g}$ ) and pore volume ( $0.009 \text{ cm}^3/\text{g}$ ), indicating weak mesoporosity, which is consistent with its type II isotherm behavior and suggests characteristics closer to those of non-porous or macroporous materials.



**Table 2.** BET surface areas and pore volumes of CPAC samples

Sample	$S_{BET}^a$ (m <sup>2</sup> /g)	$S_{mic}^b$ (m <sup>2</sup> /g)	$S_{mes}$ (m <sup>2</sup> /g)	$V_t^c$ (cm <sup>3</sup> /g)	$V_{mic}^b$ (cm <sup>3</sup> /g)	$V_{mes}$ (cm <sup>3</sup> /g)
CPAC-201	4.773	0.000	4.773	0.009	0.000	0.009
CPAC-202	198.233	0.000	198.233	0.227	0.000	0.227

<sup>a</sup> Specific surface area calculated by the BET method at  $P/P_0 = 0.05–0.30$ <sup>b</sup> Micropore evaluated by  $t$ -plot method<sup>c</sup> Total pore volume obtained from the single-point adsorption volume at  $P/P_0 = 0.995$ **Table 3.** The adsorption of BTEX using CPAC

Sample	Concentration of adsorbed BTEX on CPAC (gas, mg/L)				
	Benzene	Toluene	Etil benzene	m,p-Xylene	o-Xylene
CPAC-201	0.262	1.273	0.264	1.799	0.580
CPAC-202	0.557	6.418	0.388	1.455	0.784

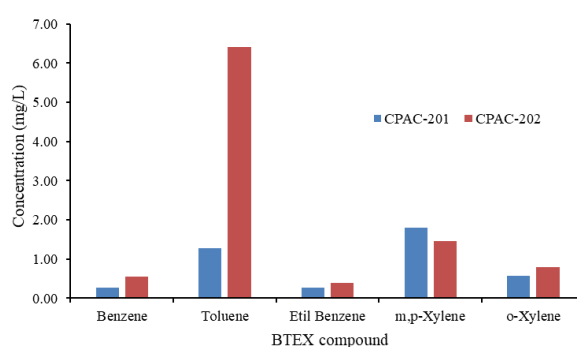
In contrast, CPAC-202 shows a significantly higher surface area of 198.233 m<sup>2</sup>/g and a well-defined mesoporous structure (Figure 5). Li *et al.* [32] reported activated carbons with extremely high surface areas, reaching ~2,000 m<sup>2</sup>/g, produced from biomass sources such as pine cones, spruce cones, larch cones, and whole spruce cones. These findings highlight that different biomass precursors can yield surface areas that vary widely. The final surface area is strongly influenced by factors such as biomass type, activation agent, activation temperature, and activation duration.

Overall, the pore characteristics obtained here show that the carbonization conditions applied to CPAC-202 were more effective in developing pore structures, resulting in a much larger surface area and a stronger mesoporous character.

### 3.4. Adsorption of BTEX

CPAC-201 and CPAC-202 were used as BTEX adsorbents at an initial concentration of 25 mg/L. The results showed that CPAC-201 achieved its highest adsorption with m,p-xylene (1.799 mg/L), while CPAC-202 showed its best performance with toluene (6.418 mg/L). These results indicate that activated carbon with a larger surface area and mesoporous character (CPAC-202) has better adsorption performance. This aligns with previous studies [33, 34], which reported that the BTEX adsorption process is strongly influenced by specific surface area, pore volume, and pore size. In this study, BTEX results were more dominant in CPAC-202, which has a larger surface area and pore volume capacity.

In the CPAC-202, the presence of C=N bonds on adsorbent surfaces generally enhances BTEX adsorption mainly through increased chemical interaction and affinity. The C=N functional groups (like amines) introduce basic sites and can form stronger interactions with the aromatic rings of BTEX by  $\pi$ - $\pi$  electron donor-acceptor interactions or hydrogen bonding, increasing adsorption capacity [35]. The C=N groups can enhance surface polarity and selectivity, improving BTEX capture from gas or aqueous phases compared to non-functionalized carbons [36].

**Figure 7.** Adsorption of BTEX using CPAC samples

## 4. Conclusion

Activated carbon from cassava peels (CPAC) was successfully synthesized through carbonization at 400°C (t: 60 minutes) followed by a dual activation stage: chemical activation (carbon: 30% H<sub>3</sub>PO<sub>4</sub>, ratio 1:5, w/w) and physical activation (furnace, T: 600°C, t: 60 minutes). The activated carbon derived from biomass, such as cassava peels, is highly regarded for its renewability and environmental friendliness (SDGs 11, 13, and 15). CPAC-201 (without carbonization) and CPAC-202 (with carbonization) have an amorphous character with functional groups that include O-H, C-H, C≡C, C=C stretching, C-O, and C=N. In the SEM-EDX section results, the surfaces of CPAC-201 and CPAC-202 are dominated by C and O elements, with a porous surface character observed on CPAC-202. The carbonization step changes pore properties. CPAC-202 (with carbonization) has a mesoporous character with a surface area up to 198.233 m<sup>2</sup>/g, and the surface is dominated by C and O elements. The selectivity of BTEX gas adsorption is more significant for toluene using CPAC-202, with the best adsorption reaching 6.418 mg/L.

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